# Stability, accuracy and time-integration issues in SPH schemes

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#### Plan of the Talk

- The standard SPH: general structure
- Weakly-compressibility assumption: issues in pressure evaluation
- Diffusive variants of SPH: main features and limits
- The  $\delta$ -SPH scheme: a consistent diffusive variant
- Current developments: the  $\delta$ LES-SPH and the  $\delta$ plus-SPH

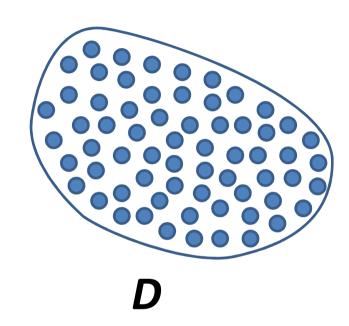
#### **General features of the SPH**

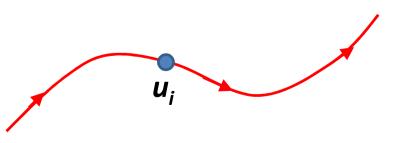
The SPH is a *particle* method

The fluid domain (*D* hereinafter) is discretized into a finite number of particles that represent elementary volumes of fluid

No topological connections => the SPH is a *Meshless* method

Particles transport the values of the physical quantities (e.g. pressure and velocity), moving with the fluid velocity => the SPH is a *Lagrangian* method





#### General features of the SPH

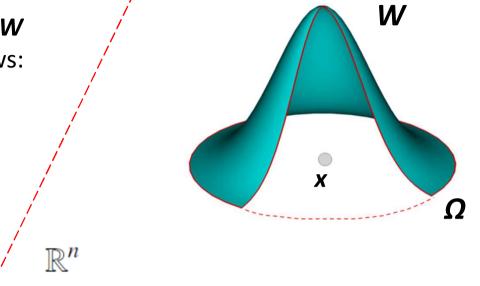
#### Why smoothing?

- the Lagrangian nature of the SPH induces non-uniform spatial distributions of particles during the flow evolution
- the absence of topological connections between particles (meshless method)
   makes the evaluation of <u>standard</u> differential operators very complex

The smoothing procedure allows us to model the interactions between neighbour particles in a simple and consistent way and to approximate the usual differential operators in a reliable manner

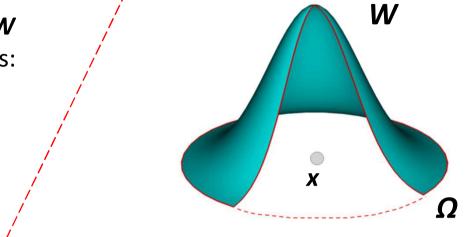
Let us consider a weight function **W** (kernel function) defined as follows:

- radial and positive
- with a compact support  $\Omega$  (i.e. it is null outside  $\Omega$ )
- C¹(Rn) at least



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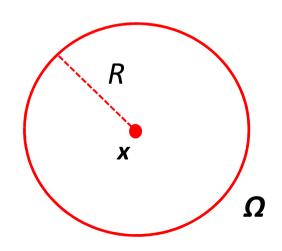
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The kernel function has generally a bump-like shape:

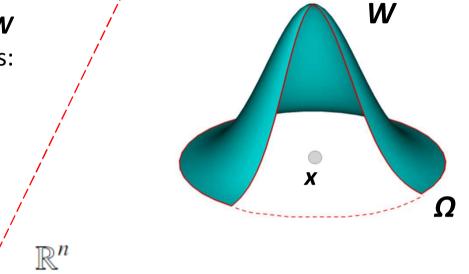
 $\mathbb{R}^n$ 

- Gaussian-type
- Polinomial type (e.g. Wendland kernels)
- Spline kernels (e.g. Cubic/quintic splines)

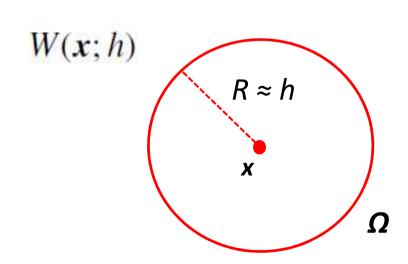


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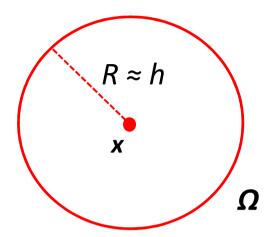
The kernel function is generally expressed as a function of a reference length h, called  $smoothing\ length$ , which is proportional to the radius R of the kernel domain  $\Omega$ 



The kernel function is normalized to one, that is:

$$\int_{\Omega} W(\mathbf{x}; h) \, \mathrm{d}V^* = 1 \qquad h > 0$$

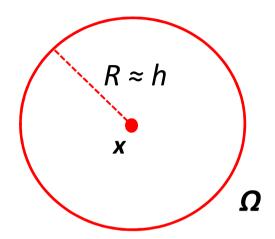
Consequently, the kernel function W preserves its «mass» inside the support  $\Omega$  for every choice of h



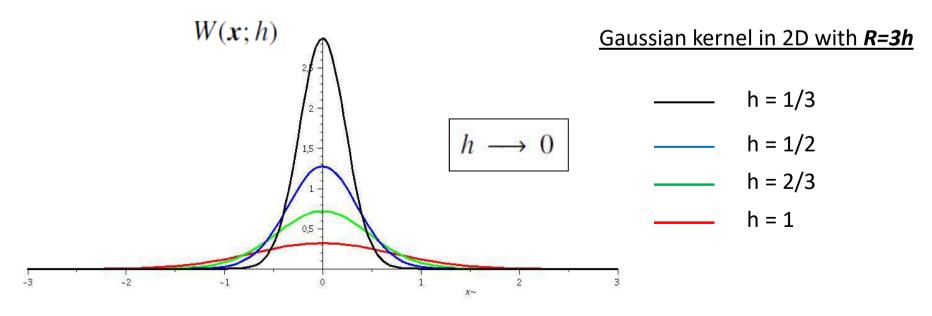
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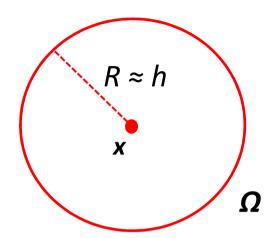
For h going to zero, the Kernel function shrinks to a point (preserving its mass)



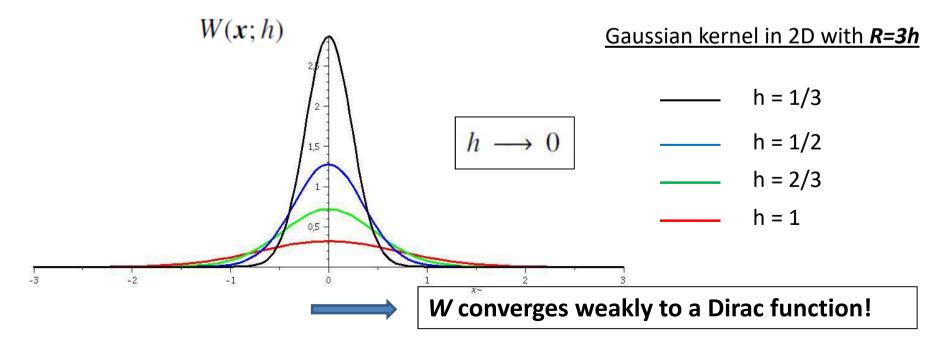
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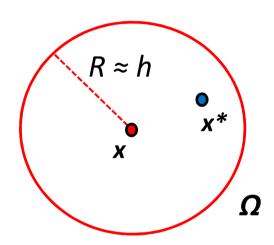


The smoothing procedure is defined through a <u>convolution integral</u> with the kernel function  $\boldsymbol{W}$  <u>over the fluid domain  $\boldsymbol{D}$ </u>

In particular, for a generic scalar function f, we define:

$$\langle f \rangle(\mathbf{x}) = \int_{\Omega \cap D} f(\mathbf{x}^*) W(\mathbf{x} - \mathbf{x}^*, h) \, \mathrm{d}V^*$$

the support  $\Omega$  is centred at the point x and the integration is done on the variable  $x^*$ 



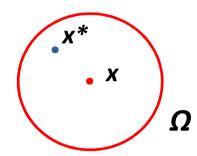
As a consequence of the properties of W, we have:

$$W(x - x^*; h) = W(x^* - x; h)$$

❖ 
$$\nabla W(x - x^*; h) = -\nabla^* W(x - x^*; h)$$
 where  $\nabla^*$  denotes differentiation with respect to  $x^*$ 

The simplest case is obtained for f=1

$$\Gamma(\mathbf{x}) = \int_{\Omega \cap D} W(\mathbf{x} - \mathbf{x}^*; h) \, \mathrm{d}V^*$$



This function takes into account how much "mass" of the fluid domain D is inside the kernel domain  $\Omega$ 

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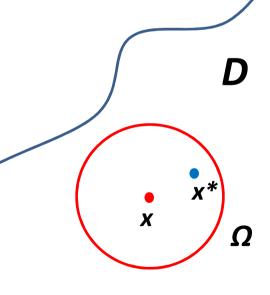
$$\Gamma(\mathbf{x}) = \int_{\Omega \cap D} W(\mathbf{x} - \mathbf{x}^*; h) \, \mathrm{d}V^*$$

This function takes into account how much "mass" of the fluid domain  ${m D}$  is inside the kernel domain  ${m \Omega}$ 

Since the kernel is normalized, we have:

$$\Gamma(x) = 1$$
 if  $\Omega \subset D$ 

All the «mass» is inside the fluid domain



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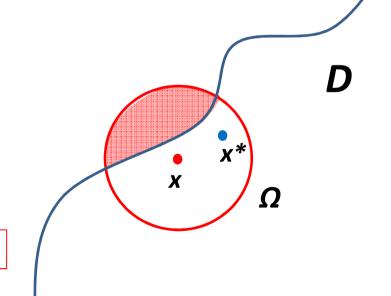
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Since the kernel is normalized, we have:

$$\Gamma(x) = 1$$
 if  $\Omega \subset D$ 

$$\Gamma(x) < 1$$
 if  $\Omega \cap D^c \neq \emptyset$ 

Some «mass» is outside the fluid domain



$$\langle f \rangle(\mathbf{x}) = \int_{\Omega \cap D} f(\mathbf{x}^*) W(\mathbf{x} - \mathbf{x}^*, h) \, \mathrm{d}V^* \qquad \Gamma(\mathbf{x}) = \int_{\Omega \cap D} W(\mathbf{x} - \mathbf{x}^*; h) \, \mathrm{d}V^*$$

A little more involved is the derivation of the smoothed gradient operator

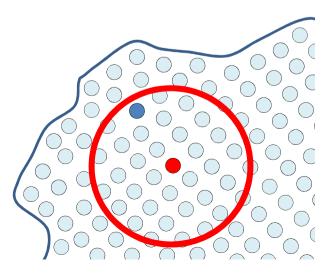
Using integration by parts (and a careful modelling of boundary terms), it is possible to obtain the following approximation:

$$\langle \nabla f \rangle (\mathbf{x}) = \int_{\Omega \cap D} [f(\mathbf{x}^*) - f(\mathbf{x})] \nabla W(\mathbf{x} - \mathbf{x}^*, h) \, dV^* + \mathcal{O}(h)$$

The fluid domain is discretized in a finite number of particles that represent elementary volumes of fluid and transport the main physical quantities

#### Let us assume that the volumes $V_i$ are known...

(these may be obtained through geometrical procedures basing on particle distribution or during the numerical simulation)



The fluid domain is discretized in a finite number of particles that represent elementary volumes of fluid and transport the main physical quantities

#### Let us assume that the volumes V<sub>i</sub> are known...

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Then, we replace the integral over  $\Omega$  by summations over the neighbour particles

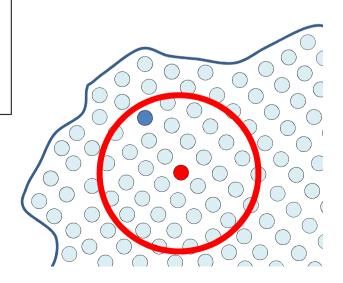
$$\Gamma(x) = \int_{\Omega \cap D} W(x - x^*; h) \, dV^* \qquad \Gamma_i = \sum_{j \in \mathcal{N}_i} W_{i,j} \, V_j$$

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$$W_{i,j} = W(x_i - x_j, h)$$

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$$\mathcal{N}_i = \left\{ j \text{ such that } ||x_i - x_j|| \le R \right\}$$



#### Similarly, we define:

$$\langle f \rangle(x) = \int_{\Omega \cap D} f(x^*) W(x - x^*, h) dV^*$$

$$\langle f \rangle_i = \sum_{j \in \mathcal{N}_i} f_j W_{i,j} V_j$$

where  $f_i = f(x_i)$ 

$$\langle \nabla f \rangle (x) \, = \, \int_{\Omega \cap D} \left[ \, f(x^*) - f(x) \, \right] \, \nabla W(x - x^*, h) \, \mathrm{d}V^* \qquad \quad \langle \nabla f \rangle_i \, = \, \sum_{j \in \mathcal{N}_i} \left( \, f_j - f_i \, \right) \, \nabla_i W_{i,j} \, V_j$$

$$\langle \nabla f \rangle_i = \sum_{j \in \mathcal{N}_i} (f_j - f_i) \nabla_i W_{i,j} V_j$$

where  $\nabla_i$  represents differentiation with respect to  $\mathbf{x}_i$ 

Hereinafter the symbol  $\mathcal{N}_i$  in the summations is understood

What about the convergence of discrete operator towards the continuous *smoothed* operators?

increasing the number of particle in  $\Omega$ 



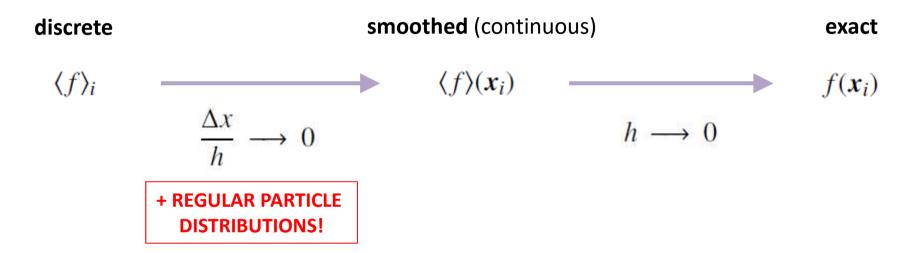
decreasing  $\Delta x/h$ 

 $\Delta x$  is the mean particle distance

In any case....

- the convergence strongly depends on the way in which the particles are distributed (regular distributions are needed)
- even in the presence of regular particle distribution, the order of convergence is generally between 1 and 2

For the function, if  $x_i \in \Omega \subset D$  (i.e. inside the fluid domain)

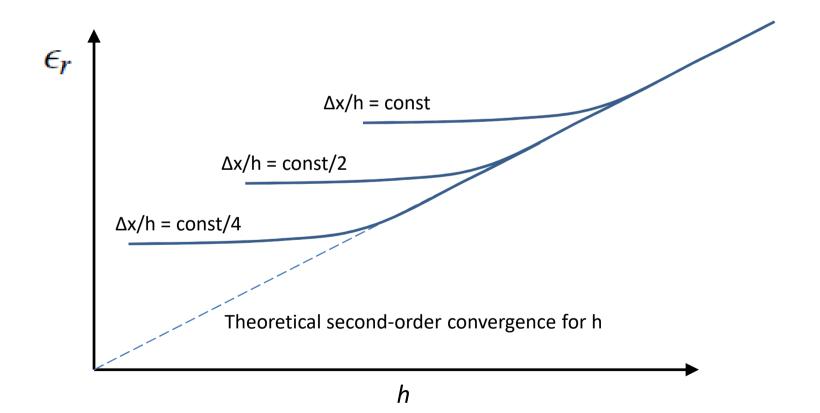


For regular distributions, the convergence to the exact solution is attained if BOTH the parameters  $\Delta x/h$  and h go to zero! (see, for example, Quinlan et al. 2006)

$$\epsilon_r \, = \, \|\, \langle f \rangle_i \, - \, f(\boldsymbol{x}_i) \, \|$$

For example, if we check the convergence of the SPH by decreasing h while  $\Delta x/h$  is fixed

(i.e. constant number of particles in  $\Omega$ )...



For 
$$x_i \in \Omega \subset D$$
 (i.e. inside the fluid domain)

for  $\Delta x/h$ ,  $h \ll 1$  ....and for regular distributions!

$$\Gamma_i = \sum_j W_{i,j} V_j \simeq 1$$

$$\langle f \rangle_i = \sum_j f_j W_{i,j} V_j \simeq \Gamma_i f(\mathbf{x}_i)$$

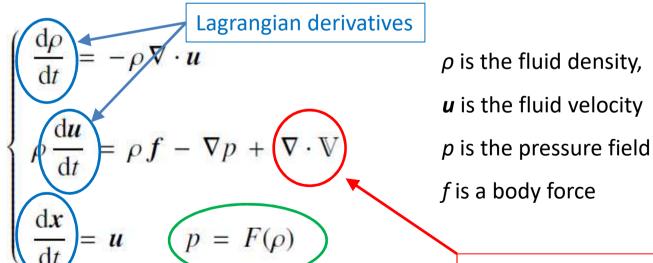
$$\nabla \Gamma_i = \sum_j \nabla_i W_{i,j} V_j \simeq 0$$

$$\langle \nabla f \rangle_i = \sum_j (f_j - f_i) \nabla_i W_{i,j} V_j \simeq \Gamma_i \nabla f(\mathbf{x}_i)$$

We are interested in the **SPH in the fluid dynamics field**....

Despite many fluids (like water) are modelled as incompressible, the SPH in its basic form relies on the hypotheses that **the fluid is weakly-compressible** (this will be clarified later)

It may be derived from the Navier-Stokes equations for compressible fluids:



State equation for barotropic fluids

viscous component of the stress tensor

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It may be derived from the Navier-Stokes equations for compressible fluids:

$$\begin{cases} \frac{\mathrm{d}\rho}{\mathrm{d}t} = -\rho \nabla \cdot u \\ \rho \frac{\mathrm{d}u}{\mathrm{d}t} = \rho f - \nabla p + \nabla \cdot \nabla \\ \frac{\mathrm{d}x}{\mathrm{d}t} = u \qquad p = F(\rho) \end{cases} \begin{cases} \frac{\mathrm{d}\rho_i}{\mathrm{d}t} = -\rho_i \langle \nabla \cdot u \rangle_i \\ \rho_i \frac{\mathrm{d}u_i}{\mathrm{d}t} = \rho_i f_i - \langle \nabla p \rangle_i + \langle \nabla \cdot \nabla \rangle_i \\ \frac{\mathrm{d}x_i}{\mathrm{d}t} = u_i \qquad p_i = F(\rho_i) \end{cases}$$

the differential operators are substituted with their smoothed (and discrete) counterparts

Divergence of the velocity...

$$\langle \nabla \cdot \boldsymbol{u} \rangle_i = \sum_j (\boldsymbol{u}_j - \boldsymbol{u}_i) \cdot \nabla_i W_{i,j} V_j$$



we need to find out the volumes!

Being a Lagrangian method, it is common practise in the standard SPH to associate a mass  $m_i$  to each particle and to maintain it constant during the flow evolution

$$\frac{\mathrm{d}m_i}{\mathrm{d}t} = 0 \qquad \text{and} \qquad V_i = \frac{m_i}{\rho_i}$$

It is also possible to define the volumes basing on geometrical considerations (e.g. particle distributions, Espanol & Revenga, 2003)

 $\frac{\mathrm{d}m_i}{\mathrm{d}t} = 0$ 

$$V_i = \frac{m_i}{\rho_i}$$

#### Generally....

- the SPH simulation is initialized by imposing a uniform particle distribution (or, at least, as regular as possible!)
  - => the volumes are <u>initially</u> uniform

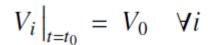
$$V_i \Big|_{t=t_0} = V_0 \quad \forall i$$

$$\frac{\mathrm{d}m_i}{\mathrm{d}t} = 0$$

$$V_i = \frac{m_i}{\rho_i}$$

#### Generally....

- the SPH simulation is initialized by imposing a uniform particle distribution (or, at least, as regular as possible!)
  - => the volumes are *initially* uniform
- the density field is assigned as an initial condition
   (and generally it is not constant all over the fluid domain)
   => the particles may have different masses
- During the simulation, the masses do not change while the density field evolves according to the physical equations
  - => volumes may evolve in a way that disregards the actual geometrical distribution of particles



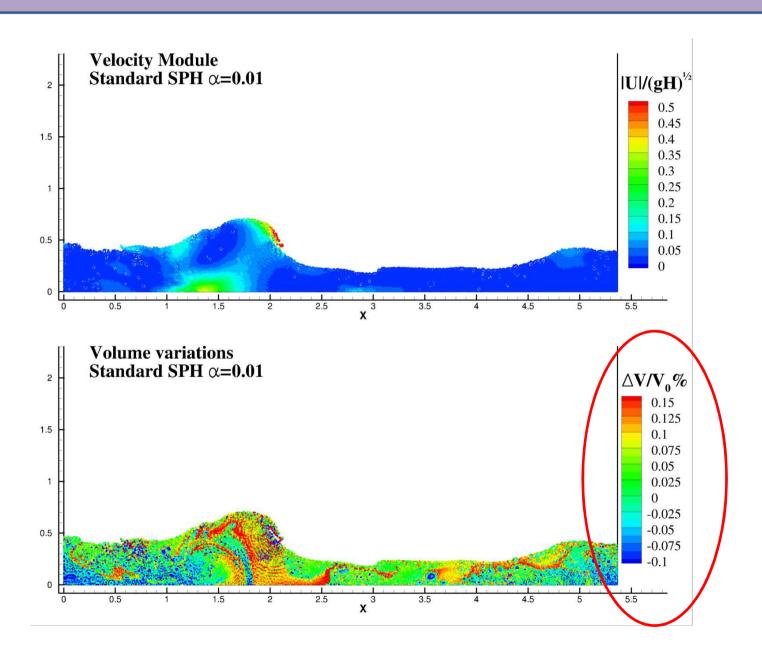


$$m_i = \rho_i \big|_{t=t_0} V_0$$



$$V_i(t) = \frac{m_i}{\rho_i(t)}$$

=> Reduced accuracy when intense density gradients occur!



About the pressure gradient....

$$\langle \nabla p \rangle_i = \sum_j (p_i + p_j) \nabla_i W_{i,j} V_j$$

- preserves linear and angular momenta
- the work along the free surface is null in an integral sense, namely

$$\int_{\partial D} p(\boldsymbol{u} \cdot \boldsymbol{n}) \, \mathrm{d}S = 0$$

#### **Advantages:**

- if we set *p*=0 along the FS at the initial time, the SPH does a null work along the FS (in an integral sense) during the subsequent evolution
- in comparison to the incompressible SPH variants, there is no need to impose p=0 along the FS during the evolution

#### Almost done...

$$\begin{cases} \frac{\mathrm{d}\rho_i}{\mathrm{d}t} = -\rho_i \sum_j (\boldsymbol{u}_j - \boldsymbol{u}_i) \cdot \nabla_i W_{i,j} V_j \\ \rho_i \frac{\mathrm{d}\boldsymbol{u}_i}{\mathrm{d}t} = \rho_i \boldsymbol{f}_i - \sum_j (p_j + p_i) \nabla_i W_{i,j} V_j + \langle \nabla \cdot \nabla \rangle_i \end{cases}$$
 Viscous term (Monaghan & Gingold,1983) 
$$\frac{\mathrm{d}\boldsymbol{x}_i}{\mathrm{d}t} = \boldsymbol{u}_i \qquad p_i = F(\rho_i)$$

Symmetric => cons. linear momentum

$$\langle \nabla \cdot \mathbb{V} \rangle_i = K \sum_j \underbrace{\frac{(u_j - u_i) \cdot (x_j - x_i)}{||x_j - x_i||^2}}_{\qquad \qquad \qquad \qquad \qquad V_j \\ V_j \\ K > 0$$

$$\sum_i u_i \cdot \langle \nabla \cdot \mathbb{V} \rangle_i V_i \leq 0 \quad \text{=>} \quad \text{purely dissipative term!}$$

$$\langle \nabla \cdot \mathbb{V} \rangle_i = K \sum_j \frac{(u_j - u_i) \cdot (x_j - x_i)}{||x_j - u_i||^2} \nabla_i W_{i,j} V_j$$
 To stabilize and regularize the simulations of "inviscid" flow

the simulations of "inviscid" flows



$$K = \begin{cases} \alpha \, h \, c_0 \, \rho_0 \\ c_0 \text{ is the sound velocity (to be defined later)} \\ \rho_0 \text{ is the reference density value} \end{cases}$$

$$n \, (n+2) \, \mu \qquad \text{PHYSICAL VISCOSITY} \qquad \mu \text{ is the dynamical vison}$$

$$n \, \text{ is the number of spatial dimensions}$$

ARTIFICIAL VISCOSITY

$$\alpha = 0.01 - 0.1$$

 $\mu$  is the dynamical viscosity *n* is the number of spatial dimensions



$$\langle \nabla \cdot \mathbb{V} \rangle_i \simeq 2 \mu \nabla (\nabla \cdot \boldsymbol{u}) + \mu \nabla^2 \boldsymbol{u} \qquad \text{for} \quad h \ll 1 \,, \quad \frac{\Delta x}{h} \ll 1 \,,$$

and regular particle distributions

If the viscosity is set to zero, the standard SPH preserves the **sum of kinetic energy**, **potential energy** (**if any**) and **reversible internal energy** 

$$\mathcal{E}_k + \mathcal{E}_p + \mathcal{E}_c = constant$$

$$\mathcal{E}_k = \sum_i m_i \frac{\|\boldsymbol{u}_i\|^2}{2} \qquad \mathcal{E}_p = -\sum_i m_i \, \phi_i \qquad \mathcal{E}_c = \sum_i m_i \, \int_{\rho_0}^{\rho_i} \frac{p(s)}{s^2} \, ds$$

If the viscosity is included in the scheme, in agreement with the second law of thermodynamics, we have:

$$\frac{\mathrm{d}}{\mathrm{d}t} \left( \mathcal{E}_k + \mathcal{E}_p + \mathcal{E}_c \right) = \mathcal{P} \leq 0$$

Power due to dissipation

Up to now, the SPH equations represent a generic compressible fluid

$$\begin{cases} \frac{\mathrm{d}\rho_{i}}{\mathrm{d}t} = -\rho_{i} \sum_{j} (\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot \nabla_{i} W_{i,j} V_{j} \\ \\ \rho_{i} \frac{\mathrm{d}\boldsymbol{u}_{i}}{\mathrm{d}t} = \rho_{i} \boldsymbol{f}_{i} - \sum_{j} (p_{j} + p_{i}) \nabla_{i} W_{i,j} V_{j} + K \sum_{j} \frac{(\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot (\boldsymbol{x}_{j} - \boldsymbol{x}_{i})}{\|\boldsymbol{x}_{j} - \boldsymbol{x}_{i}\|^{2}} \nabla_{i} W_{i,j} V_{j} \\ \\ \frac{\mathrm{d}\boldsymbol{x}_{i}}{\mathrm{d}t} = \boldsymbol{u}_{i} \qquad p_{i} = F(\rho_{i}) \end{cases}$$

The fluid is barotropic, then the pressure field is derived from the knowledge of the density field

The signals (e.g. pressure waves) move with a finite velocity, which is called **sound velocity**  $c(\rho)$ 

$$c^2(\rho) = \frac{\mathrm{d}p}{\mathrm{d}\rho} = \frac{\mathrm{d}F(\rho)}{\mathrm{d}\rho}$$

For the problems we want to simulate (e.g. water), the physical sound velocity is much larger than the fluid velocity

⇒ nearly incompressible fluids (small density variations)!

=> we can linearize the state equation around a reference density value  $\rho_o$ 

$$p = F(\rho) \longrightarrow p = c_0^2 (\rho - \rho_0)$$
 where  $c_0 = c(\rho_0)$ 

Generally for free-surface flows  $\rho_0$  is the density along the FS (where p=0)

The time step of the SPH is approximately

$$\Delta t \simeq \frac{h}{c_0}$$

Unfortunately, we cannot use the physical sound velocity otherwise the time step of the simulation (which depends on the inverse of  $c_0$ ) would be too small!

$$c_0 = 10 \max \left( U_{max}, \sqrt{\frac{\Delta p_{max}}{\rho_0}} \right)$$

where  $U_{max}$  and  $p_{max}$  are the maximum expected velocity and pressure

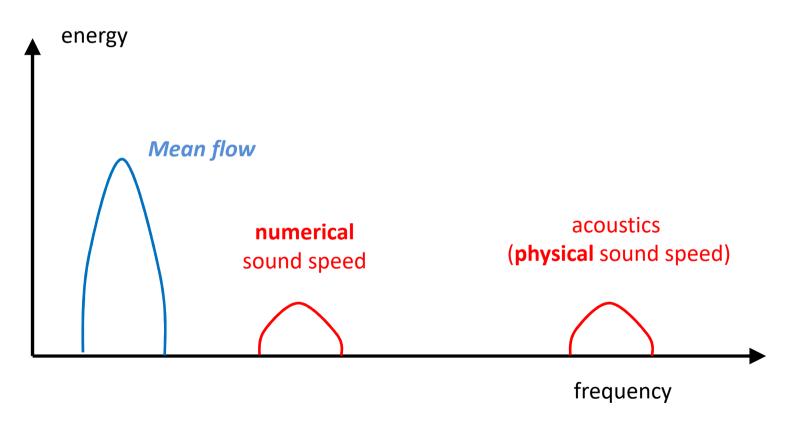
The above constraint guarantees that the density variations maintains below 1% during the evolution, that is:

$$\left| \frac{\Delta \rho}{\rho} \right| \le 0.01$$

Weakly-compressibility assumption

In fact, the use of a *numerical sound velocity* is not a problem...

...at least for the phenomena we want to simulate!



# The standard SPH - weak-compressibility

Finally.... the standard SPH scheme

$$\begin{cases} \frac{\mathrm{d}\rho_{i}}{\mathrm{d}t} = -\rho_{i} \sum_{j} (\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot \nabla_{i} W_{i,j} V_{j} \\ \\ \rho_{i} \frac{\mathrm{d}\boldsymbol{u}_{i}}{\mathrm{d}t} = \rho_{i} \boldsymbol{f}_{i} - \sum_{j} (p_{j} + p_{i}) \nabla_{i} W_{i,j} V_{j} + K \sum_{j} \frac{(\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot (\boldsymbol{x}_{j} - \boldsymbol{x}_{i})}{\|\boldsymbol{x}_{j} - \boldsymbol{x}_{i}\|^{2}} \nabla_{i} W_{i,j} V_{j} \\ \\ \frac{\mathrm{d}\boldsymbol{x}_{i}}{\mathrm{d}t} = \boldsymbol{u}_{i} \qquad p_{i} = c_{0}^{2} (\rho_{i} - \rho_{0}) \qquad V_{i} = m_{i}/\rho_{i} \end{cases}$$

- ✓ Conservation of mass
- ✓ Conservation of linear and angular momenta
- ✓ If K=0, conservation of (kinetic + potential + internal)

(see, for example, Monaghan 2005)

# The standard SPH - weak-compressibility

### The standard SPH:

### PROS:

- ✓ explicit scheme => good for parallelization (e.g. 3D simulations)
- ✓ Implicit fulfilment of the free-surface boundary conditions
  - => good for simulations with complex interface deformations/fragmentations

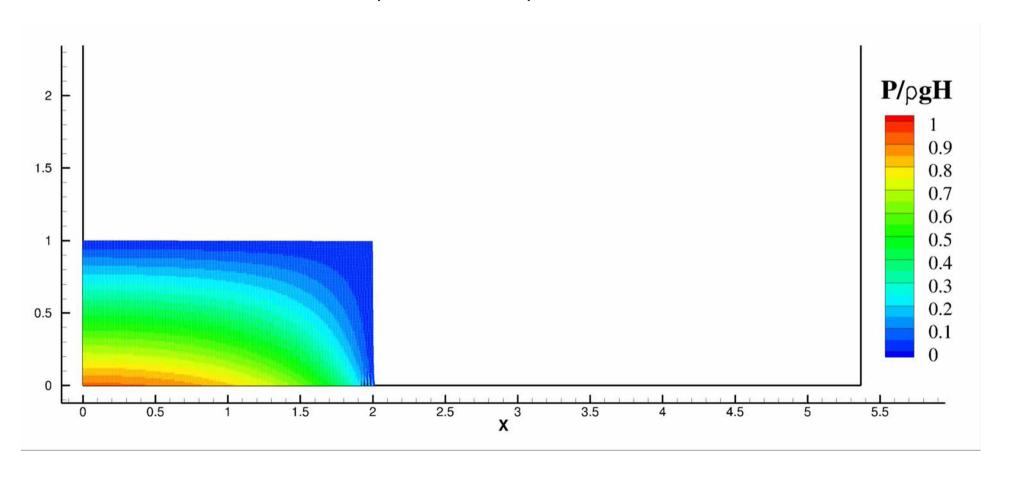
### CONS:

- large sound speed => small time step
- weakly-compressible fluid => acoustic noise
- > central-explicit scheme (+ nonlinearities) => spurious numerical noise

numerical schemes to reduce/avoid the spurious numerical noise

Generally, the velocity field and particle positions are good....

What about other relevant quantities like pressure?

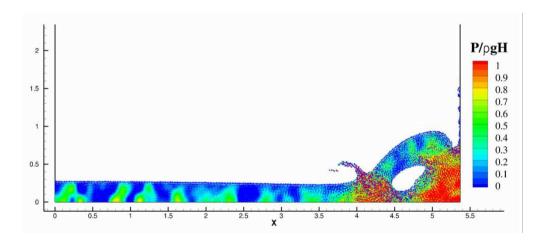


Dam-break flow: "inviscid fluid" simulated with artificial viscosity ( $\alpha$ =0.01)

Kinematics is correct, but pressure field is noisy!

Main sources of noise on the pressure field:

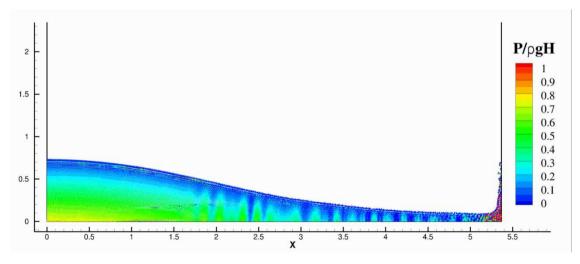
Numerical scheme: centred + explicit



Kinematics is correct, but pressure field is noisy!

Main sources of noise on the pressure field:

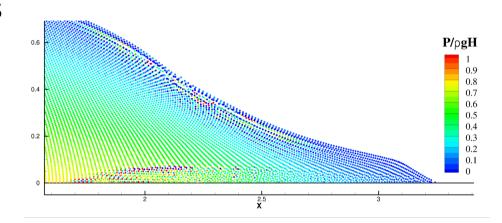
- Numerical scheme: centred + explicit
- Physical model: acoustic waves



Kinematics is correct, but pressure field is noisy!

Main sources of noise on the pressure field:

- Numerical scheme: centred + explicit
- Physical model: acoustic waves
- Lagrangian character: particle resettlement



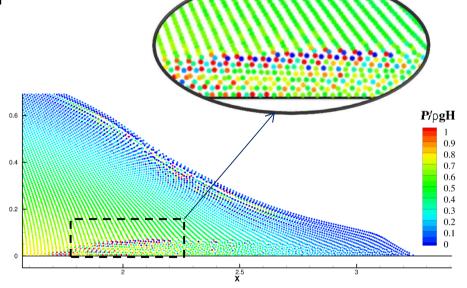
Kinematics is correct, but pressure field is noisy!

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 particle resettlement



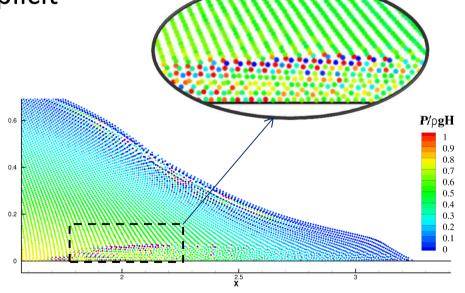
Kinematics is correct, but pressure field is noisy!

Main sources of noise on the pressure field:

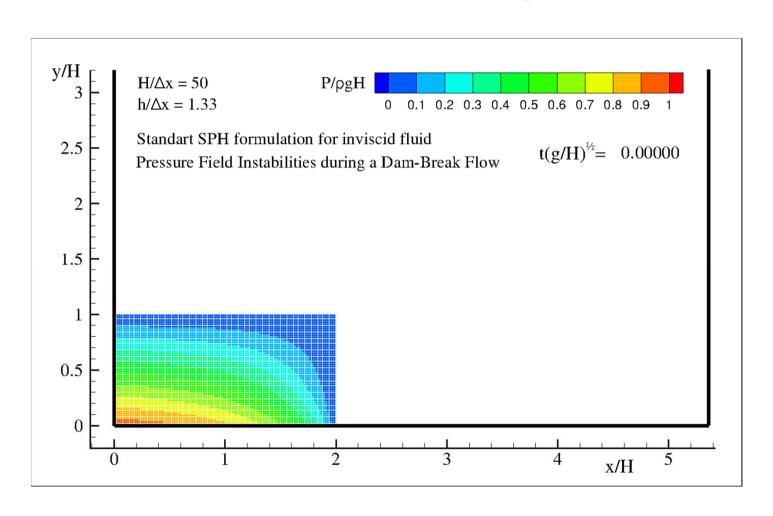
Numerical scheme: centred + explicit

- Physical model: acoustic waves
- Lagrangian character: particle resettlement

All the three aspects are strictly linked!

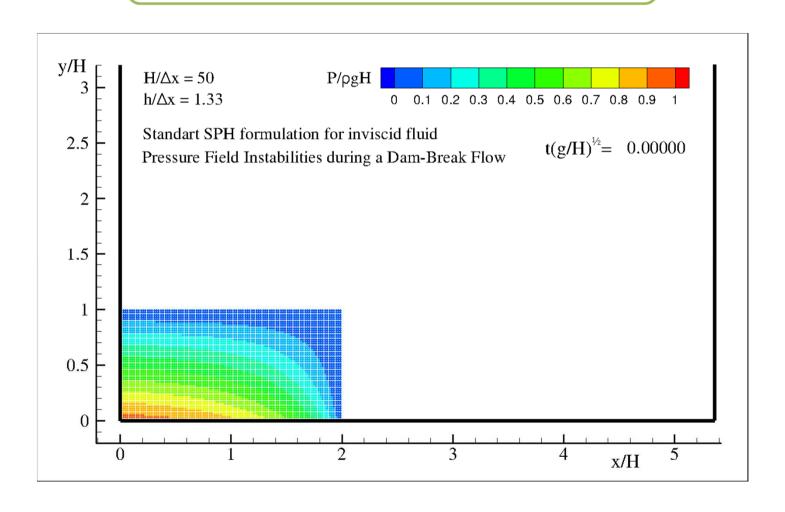


An example: simulation of dam-break without artificial viscosity ( $\alpha=0$ )



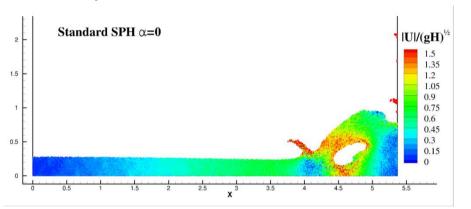
Remember the scheme relies on conservation:

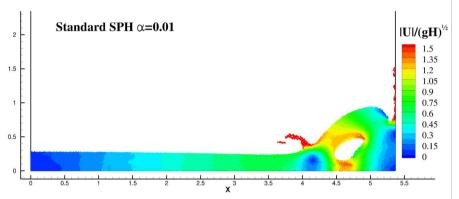
errors goes in internal energy!



The effect of the artificial viscosity is to add diffusion inside the momentum equation

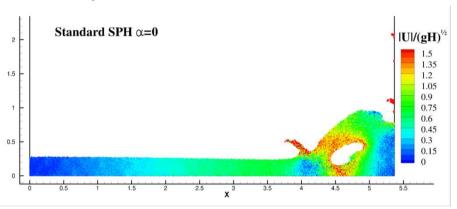
### Velocity Field

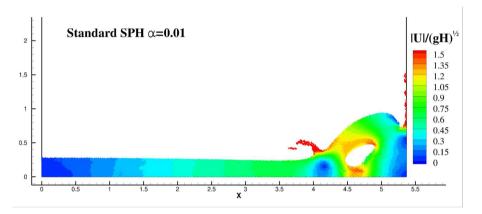




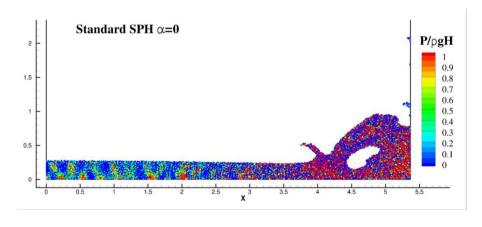
The effect of the artificial viscosity is to add diffusion inside the momentum equation

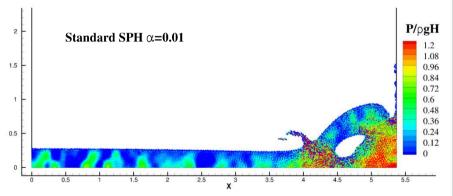
### Velocity Field





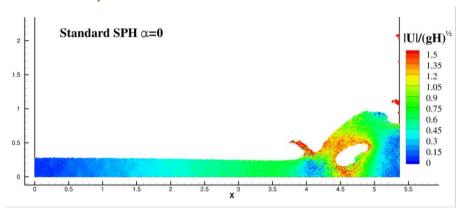
### Pressure Field

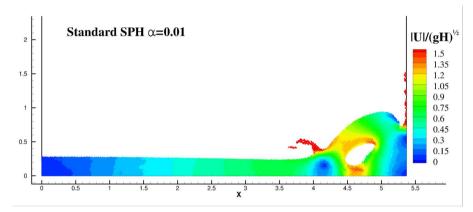




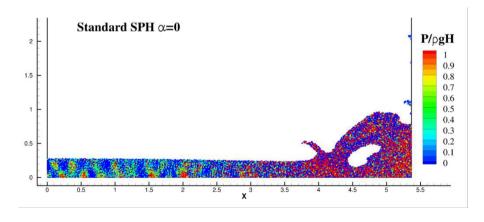
The effect of the artificial viscosity is to add diffusion inside the momentum equation

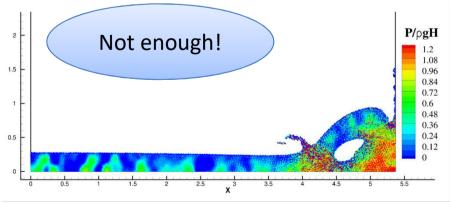
### Velocity Field





### Pressure Field





Since the spurious noise mainly affects the density/pressure fields, a possible strategy is to add a diffusive term inside the continuity equation:

$$\begin{cases} \frac{\mathrm{d}\rho_{i}}{\mathrm{d}t} = -\rho_{i} \sum_{j} (\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot \nabla_{i} W_{i,j} V_{j} + \delta h c_{0} \mathcal{D}_{i} \\ \rho_{i} \frac{\mathrm{d}\boldsymbol{u}_{i}}{\mathrm{d}t} = \rho_{i} \boldsymbol{f}_{i} - \sum_{j} (p_{j} + p_{i}) \nabla_{i} W_{i,j} V_{j} + K \sum_{j} \frac{(\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot (\boldsymbol{x}_{j} - \boldsymbol{x}_{i})}{\|\boldsymbol{x}_{j} - \boldsymbol{x}_{i}\|^{2}} \nabla_{i} W_{i,j} V_{j} \\ \frac{\mathrm{d}\boldsymbol{x}_{i}}{\mathrm{d}t} = \boldsymbol{u}_{i} \qquad p_{i} = c_{0}^{2} (\rho_{i} - \rho_{0}) \qquad V_{i} = m_{i}/\rho_{i} \end{cases}$$

where  $\delta$  is a dimensionless parameter and

$$\mathcal{D}_i = 2 \sum_j \psi_{i,j} \cdot \nabla_i W_{i,j} V_j$$

the specific form of  $\psi_{i,j}$  characterizes the diffusive scheme at hand

The vector  $\psi_{i,j}$  has to be **symmetric**, that is

$$\psi_{i,j} = \psi_{j,i} \qquad \sum_{i} \mathcal{D}_{i} V_{i} = 0$$

This ensures the consistency of the integral form of the continuity equation (e.g. consistency with the equation of mass conservation)

with diffusion 
$$\sum_i \left[ \frac{\mathrm{d} \rho_i}{\mathrm{d} t} + \rho_i \langle \nabla \cdot \boldsymbol{u} \rangle_i - \delta \, h \, c_0 \, \mathcal{D}_i \right] V_i = \sum_i \left[ \frac{\mathrm{d} \rho_i}{\mathrm{d} t} + \rho_i \langle \nabla \cdot \boldsymbol{u} \rangle_i \right] V_i$$
 
$$\simeq \int_D \left[ \frac{\mathrm{d} \rho}{\mathrm{d} t} + \rho \, \nabla \cdot \boldsymbol{u} \right] \mathrm{d} V = 0$$

$$\psi_{i,j} = (\rho_j - \rho_i) \frac{(x_j - x_i)}{\|x_j - x_i\|^2}$$
 Molteni & Colagrossi (2009) 
$$\mathcal{D}_i \simeq \nabla^2 \rho_i$$
 
$$\psi_{i,j} = (\rho_j - \rho_i) \frac{(x_j - x_i)}{2h \|x_i - x_i\|}$$
 Ferrari et al. (2009)

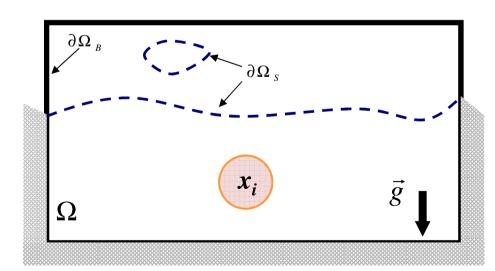
but they are inconsistent close to the free surface (no hydrostatic solution!)

For example, let us consider the diffusive term by Molteni & Colagrossi (2009)

$$2\sum_{i}(\rho_{j}-\rho_{i})\frac{(x_{j}-x_{i})}{\|x_{j}-x_{i}\|^{2}}\cdot\nabla_{i}W_{ij}V_{j}=2\nabla\rho_{i}\cdot\nabla\Gamma_{i}+\Gamma_{i}\Delta\rho_{i}+\mathcal{O}(h)$$

$$\Gamma_i = \sum_j W_{i,j} V_j \simeq 1$$

$$\nabla \Gamma_i = \sum_j \nabla_i W_{i,j} \, V_j \simeq 0$$



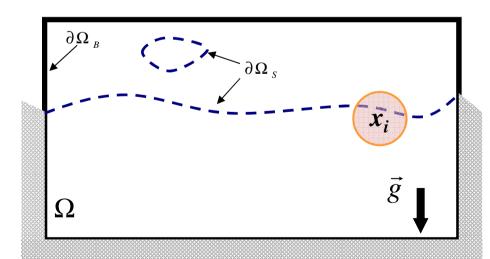
For example, let us consider the diffusive term by Molteni & Colagrossi (2009)

$$2 \sum_{i} (\rho_{j} - \rho_{i}) \frac{(\boldsymbol{x}_{j} - \boldsymbol{x}_{i})}{\|\boldsymbol{x}_{j} - \boldsymbol{x}_{i}\|^{2}} \cdot \nabla_{i} W_{ij} V_{j} = 2 \nabla \rho \left( \cdot \nabla \Gamma_{i} \right) + \Gamma_{i} \Delta \rho_{i} + \mathcal{O}(h)$$

$$\Gamma_i = \sum_j W_{i,j} V_j < 1$$

$$\nabla \Gamma_i = \sum_j \nabla_i W_{i,j} V_j \simeq \left( \mathcal{O}(h^{-1}) \right)$$

A spurious term appears close to the free surface!



To avoid such an inconsistency, Antuono et al. (2010) defined the following form:

$$\psi_{i,j} = \left[ (\rho_j - \rho_i) \left( \frac{1}{2} \left( \langle \nabla \rho \rangle_j^L + \langle \nabla \rho \rangle_i^L \right) \cdot (\boldsymbol{x}_j - \boldsymbol{x}_i) \right) \frac{(\boldsymbol{x}_j - \boldsymbol{x}_i)}{\|\boldsymbol{x}_j - \boldsymbol{x}_i\|^2} \right]$$

- this formulation is consistent close to the free surface
- the diffusive term converges to zero if h goes to zero

Inside the fluid domain

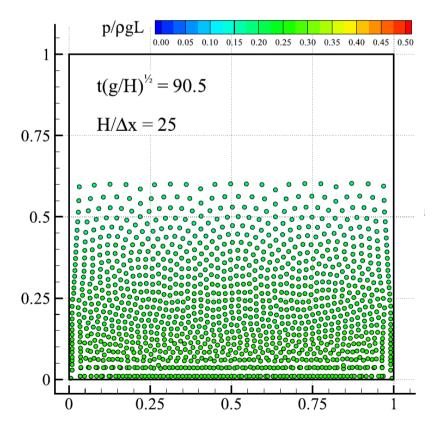
$$\mathcal{D}_i \simeq \frac{h^2}{12} \mathbb{B}_{jkpq} \left( \frac{\partial^4 \rho_i}{\partial x_j \partial x_k \partial x_p \partial x_q} \right)$$

The latter scheme is called  $\delta$ -SPH scheme

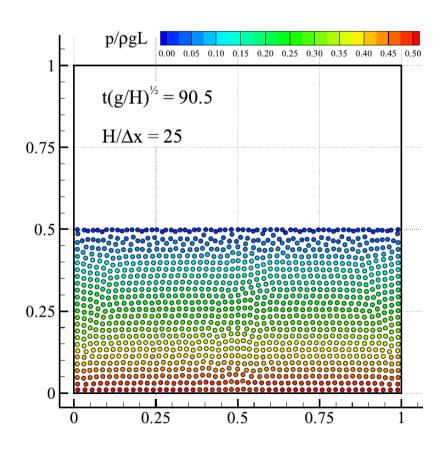
# Hydrostatic test

Molteni & Colagrossi (2009)

$$\psi_{ij} = 2 \left(\rho_j - \rho_i\right) \frac{(\boldsymbol{r}_j - \boldsymbol{r}_i)}{|\boldsymbol{r}_j - \boldsymbol{r}_i|^2}$$



### δ-SPH

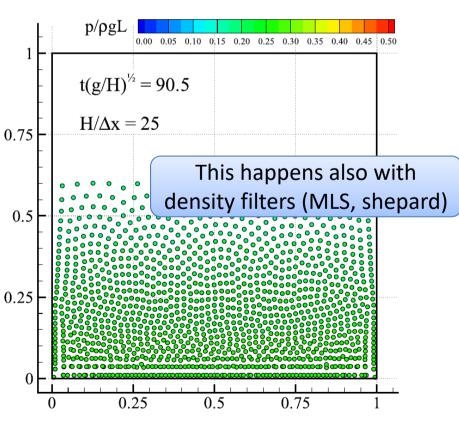


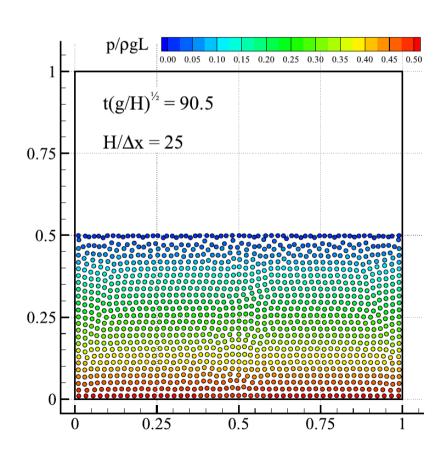
# Hydrostatic test

Molteni & Colagrossi (2009)

$$\psi_{ij} = 2 (\rho_j - \rho_i) \frac{(\boldsymbol{r}_j - \boldsymbol{r}_i)}{|\boldsymbol{r}_j - \boldsymbol{r}_i|^2}$$

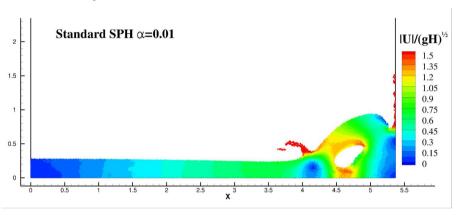
δ-SPH

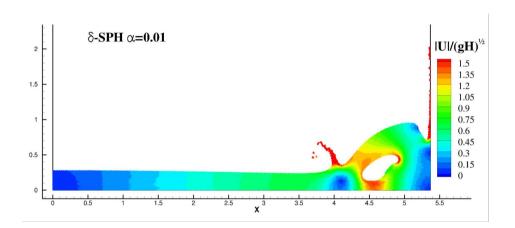




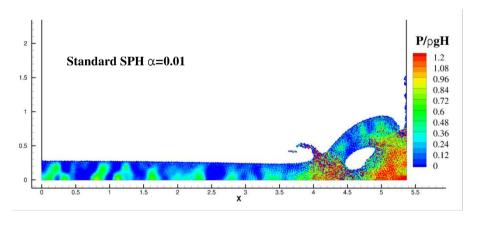
### Comparison with standard SPH

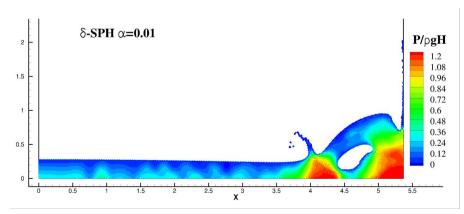
### Velocity Field

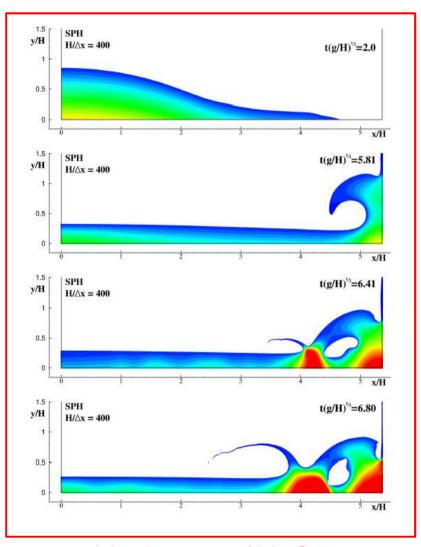




### Pressure Field







LS-FVM y/H  $H/\triangle x = 400$ 0 0.1 0.2 0.3 0.4 0.5 0.6 0.7 0.8 0.9 1 0.5 LS-FVM y/H  $H/\Delta x = 400$ 0.5 LS-FVM y/H  $H/\triangle x = 400$ 0.5 LS-FVM y/H  $H/\Delta x = 400$ 0.5

Weakly-Compressible δ-SPH

**Incompressible FVM** 

### The δ-SPH scheme

$$\begin{cases} \frac{\mathrm{d}\rho_{i}}{\mathrm{d}t} = -\rho_{i} \sum_{j} (\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot \nabla_{i} W_{i,j} V_{j} + \delta h c_{0} \mathcal{D}_{i} \\ \\ \rho_{i} \frac{\mathrm{d}\boldsymbol{u}_{i}}{\mathrm{d}t} = \rho_{i} f_{i} - \sum_{j} (p_{j} + p_{i}) \nabla_{i} W_{i,j} V_{j} + K \sum_{j} \frac{(\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot (\boldsymbol{x}_{j} - \boldsymbol{x}_{i})}{\|\boldsymbol{x}_{j} - \boldsymbol{x}_{i}\|^{2}} \nabla_{i} W_{i,j} V_{j} \\ \\ \frac{\mathrm{d}\boldsymbol{x}_{i}}{\mathrm{d}t} = \boldsymbol{u}_{i} \qquad p_{i} = c_{0}^{2} (\rho_{i} - \rho_{0}) \qquad V_{i} = m_{i}/\rho_{i} \end{cases}$$

where  $\delta$  is a dimensionless parameter and

$$\begin{split} \mathcal{D}_i &= 2 \sum_j \psi_{i,j} \cdot \nabla_i W_{i,j} \, V_j \\ \psi_{i,j} &= \left[ (\rho_j - \rho_i) - \frac{1}{2} \left( \langle \nabla \rho \rangle_j^L + \langle \nabla \rho \rangle_i^L \right) \cdot (\boldsymbol{x}_j - \boldsymbol{x}_i) \right] \frac{(\boldsymbol{x}_j - \boldsymbol{x}_i)}{\|\boldsymbol{x}_j - \boldsymbol{x}_i\|^2} \end{split}$$

# The δ-SPH scheme

The  $\delta$ -SPH maintains all the conservation properties of the standard SPH scheme

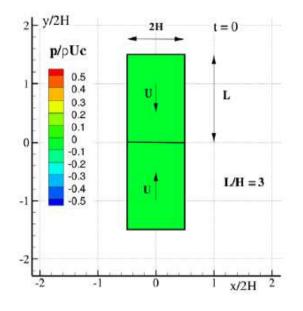
- ✓ Conservation of mass
- ✓ Conservation of linear and angular momenta
- ✓ If K=0, conservation of (kinetic + potential + internal)

(see, for example, Antuono et al. 2015)

The dimensionless parameter  $\delta$  varies in a narrow range of values that depends on the ratio  $(\Delta x/h)$  and on the spatial dimensions (see Antuono et al. 2012)

( $\delta$ =0.1 is a reliable choice in 2D simulations)

# The $\delta$ -SPH scheme – an example of application



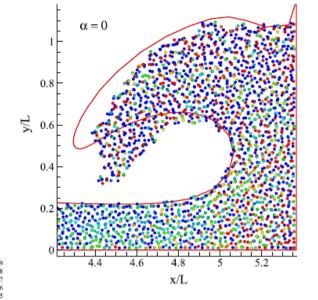
acoustic waves

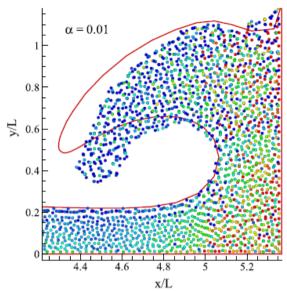
nonlinear wave-wave interaction spurious high-frequency noise

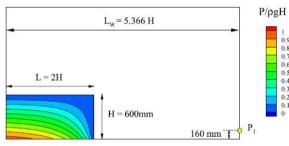
Fig. 14. The impact of two rectangular fluid patches: sketches of the evolution. The upper part of the fluid domain is given by the  $\delta$ -SPH while the lower part is obtained by using the standard SPH.

### Simulation of a dam break flow

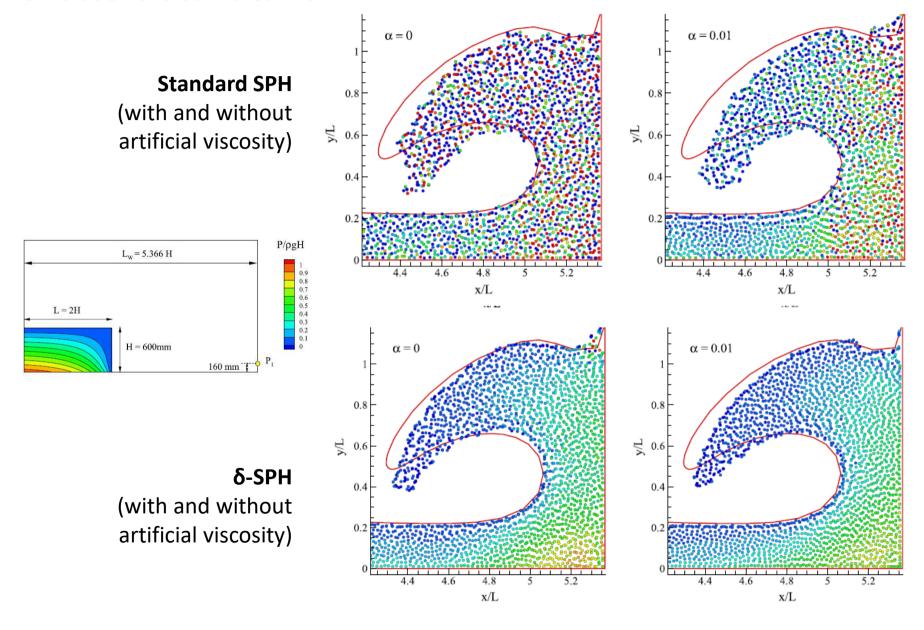
**Standard SPH** (with and without artificial viscosity)







### Simulation of a dam break flow



### The $\delta$ -SPH scheme – numerical details

$$\psi_{i,j} = \left[ (\rho_j - \rho_i) - \left( \frac{1}{2} \left( \langle \nabla \rho \rangle_j^L + \langle \nabla \rho \rangle_i^L \right) \cdot (x_j - x_i) \right) \right] \frac{(x_j - x_i)}{\|x_j - x_i\|^2}$$

An additional loop is needed in order to calculate renormalized gradients

$$\langle \nabla \rho \rangle_i^L = \sum_j \left( \rho_j - \rho_i \right) \boldsymbol{L}_i \, \nabla_i W_{ij} \, V_j \qquad \boldsymbol{L}_i = \left[ \sum_j \left( \boldsymbol{r}_j - \boldsymbol{r}_i \right) \otimes \nabla_i W_{ij} \, V_j \right]^{-1}$$

• However when using higher-order time integrators (e.g. RK4) this cost can be drastically reduced through a "frozen" diffusion

### The $\delta$ -SPH scheme – numerical details

The discrete scheme can be represented as follows:

$$\frac{\mathrm{d}\boldsymbol{w}}{\mathrm{d}t} = \boldsymbol{Q}(\boldsymbol{w}) + \boldsymbol{D}(\boldsymbol{w})$$

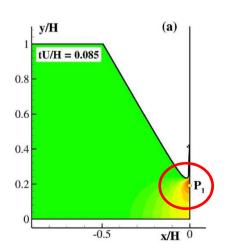
where **D(w)** contains the diffusive term

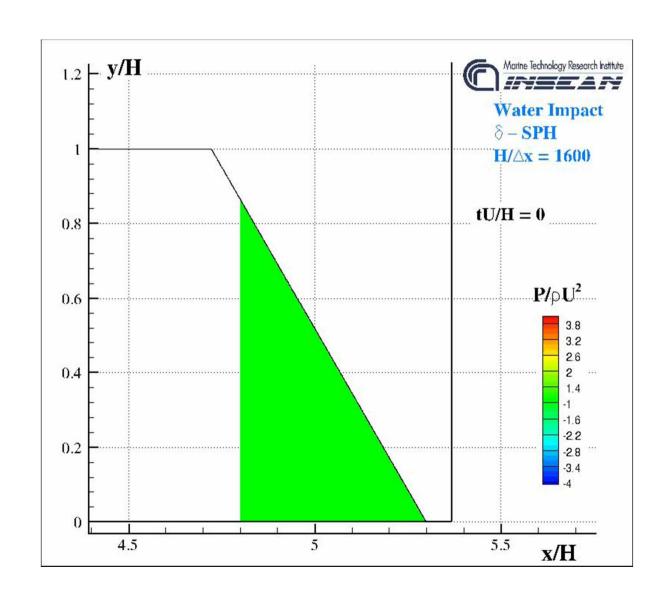
The RK 4-th order with frozen diffusion reads:

$$\begin{cases} \mathbf{w}^{(0)} = \mathbf{w}^{n} \\ \mathbf{w}^{(1)} = \mathbf{w}^{(0)} + \mathbf{Q}(\mathbf{w}^{(0)}) \Delta t / 2 + \mathbf{D}(\mathbf{w}^{(0)}) \Delta t / 2 \\ \mathbf{w}^{(2)} = \mathbf{w}^{(0)} + \mathbf{Q}(\mathbf{w}^{(1)}) \Delta t / 2 + \mathbf{D}(\mathbf{w}^{(0)}) \Delta t / 2 \\ \mathbf{w}^{(3)} = \mathbf{w}^{(0)} + \mathbf{Q}(\mathbf{w}^{(2)}) \Delta t + \mathbf{D}(\mathbf{w}^{(0)}) \Delta t \\ \mathbf{w}^{(4)} = \mathbf{w}^{(0)} + \left[ \mathbf{Q}(\mathbf{w}^{(0)}) + 2 \mathbf{Q}(\mathbf{w}^{(1)}) + 2 \mathbf{Q}(\mathbf{w}^{(1)}) + 2 \mathbf{Q}(\mathbf{w}^{(2)}) + \mathbf{Q}(\mathbf{w}^{(3)}) \right] \Delta t / 6 + \mathbf{D}(\mathbf{w}^{(0)}) \Delta t \\ \mathbf{w}^{n+1} = \mathbf{w}^{(4)}. \end{cases}$$

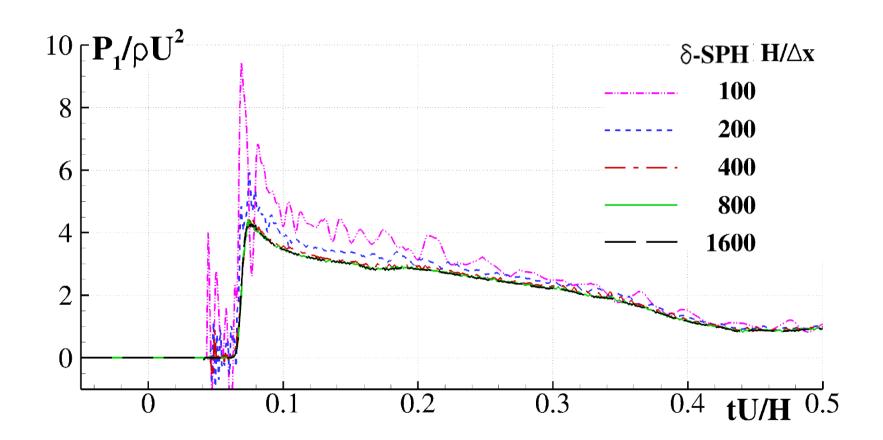
# Impinging jet

Water wedge impact against a wall

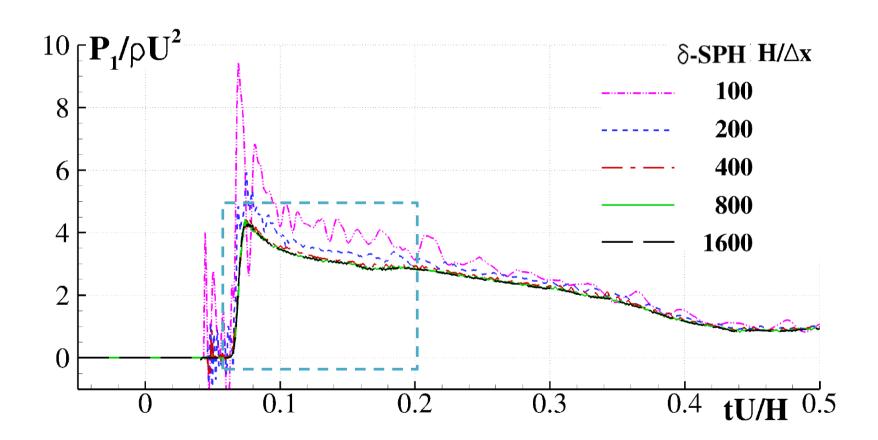


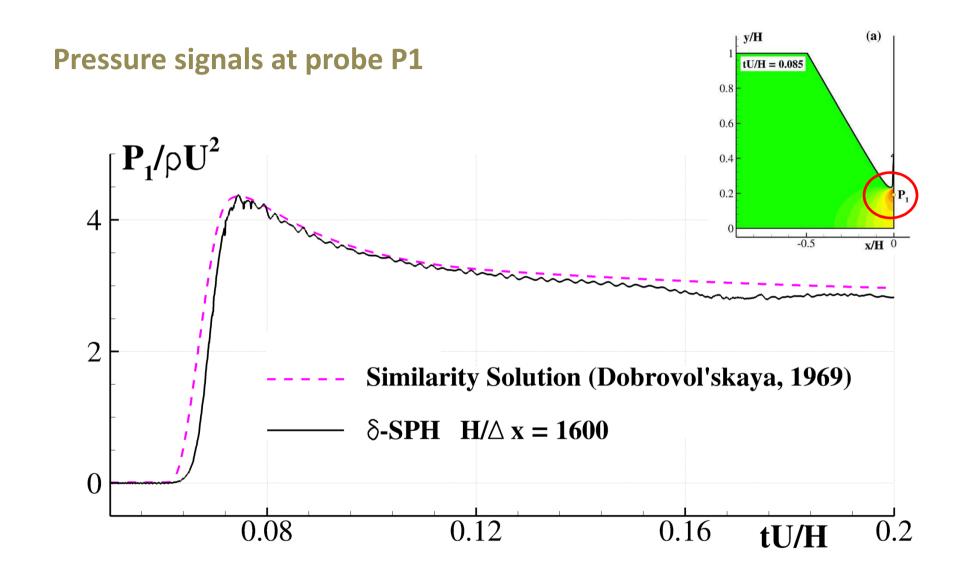


# Pressure signals at probe P1



# Pressure signals at probe P1



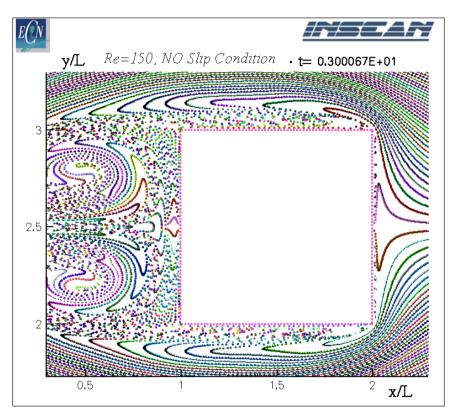


# Being Lagrangian is a double-edged sword...

Particles distribution becomes non-uniform → larger errors!

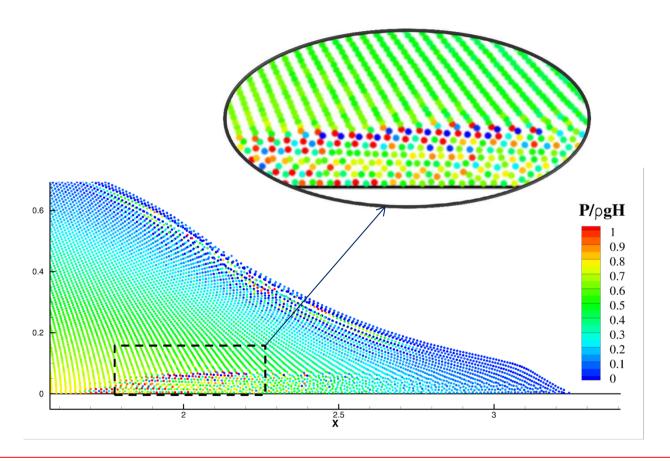
### This occurs when:

- increasing diffusion (Riemann)
- Increasing accuracy (e.g. interpolation order)
- simulating high shear regions



Eulerian solver with Lagrangian tracers

SPH has a self-rearrangement mechanism (when p is positive!)



but this induces however numerical noise and energy dissipation!!

### further insight....

$$\langle \nabla p \rangle_i = \sum_j (p_j + p_i) \nabla_i W_{i,j} V_j = \sum_j (p_j - p_i) \nabla_i W_{i,j} V_j + 2 p_i \nabla \Gamma_i$$

$$\nabla \Gamma_i = \sum_j \nabla_i W_{i,j} V_j$$

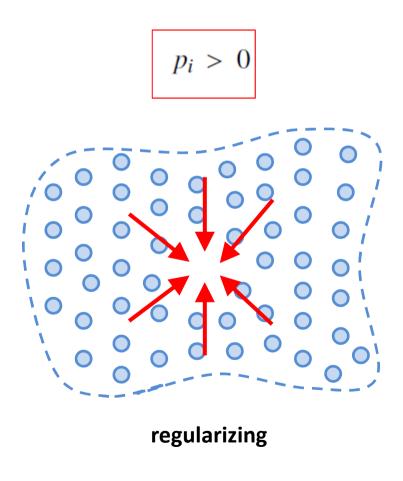
standard formula for the gradient (e.g. divergence of the velocity)

 $\nabla \Gamma_i$  points towards the «voids» in the fluid domain

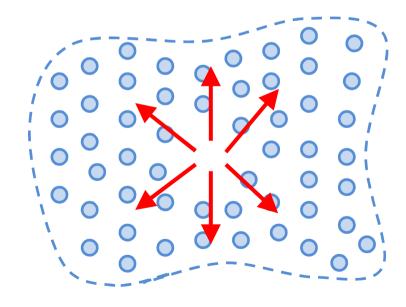
- if  $p_i > 0$ , the term  $p_i \nabla \Gamma_i$  tends to reduce the disorder in the particle distribution **wimplicit particle packing**»
- if  $p_i < 0$ , the term  $p_i \nabla \Gamma_i$  tends to increase the disorder in the particle distribution tensile instability

Inside the momentum equation, the contribution from this term is

$$-2 p_i \nabla \Gamma_i$$



$$p_i < 0$$



increasing disorder

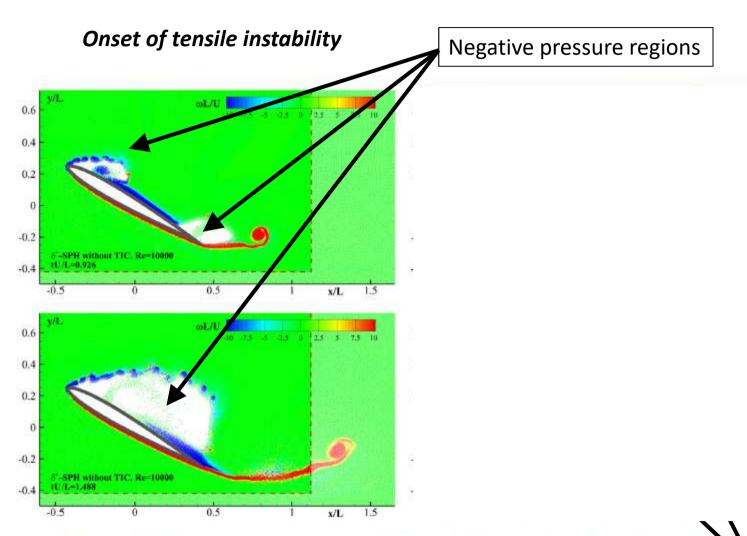


Fig. 1. Flow around a NACA0010 profile,  $\alpha=30^\circ$ , Re =10,000. Snapshots of the  $\delta^+$ -SPH solutions without (left) and with (right) Tensile Instablity Control

With tensile instability control

The idea is to put a term similar to  $-2 p_i \nabla \Gamma_i$  with  $p_i > 0$  directly in the particle position update:

"particle shifting" (Nestor et al. JCP 2009, Lind et al. JCP 2012)

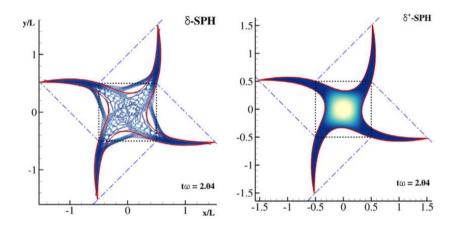
$$\begin{cases} \boldsymbol{r}_{i}^{*} = \boldsymbol{r}_{i} + \delta \boldsymbol{r}_{i} \\ \delta \boldsymbol{r}_{i} := -\text{CFL} \cdot \text{Ma} \cdot (2 h_{ij})^{2} \end{cases} \underbrace{\sum_{j} \nabla_{i} W_{ij} V_{j}}^{\text{V}_{i}}$$

$$V \Gamma_{i} = \sum_{j} \nabla_{i} W_{i,j} V_{j}$$

Increasing accuracy through particle shifting

technique: the  $\delta^+$ -SPH

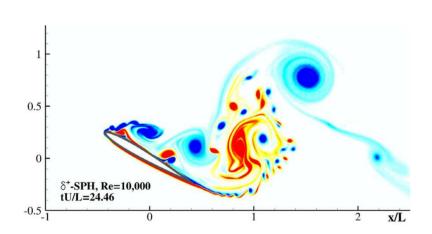
Rotating square patch Sun et al. CMAME 2016



Tensile instability control

Airfoil in stall configuration at Re=10000

Sun et al. CPC 2018



• Arbitrary Lagrangian Eulerian framework for  $\delta$ -SPH

• δ-SPH for multi-phase flows

Large Eddy Simulation perspective for δ-SPH

Di Mascio et al. (2017) Meringolo et al. (2018)

The viscous term in the momentum equation and the diffusive term in the continuity equation are interpreted as closures in the **LES framework** 

=> dynamic choice of coefficients using the velocity deformation tensor

$$\begin{cases} \frac{D\rho_{i}}{Dt} = -\rho_{i} \sum_{j} (\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot \nabla_{i} W_{ij} V_{j} + hc_{0} \sum_{j} \delta_{ij} \mathcal{D}_{ij} \cdot \nabla_{i} W_{ij} V_{j}, \\ \frac{D\boldsymbol{u}_{i}}{Dt} = \boldsymbol{g}_{i} - \frac{1}{\rho_{i}} \sum_{j} \left( p_{i} + p_{j} \right) \nabla_{i} W_{ij} V_{j} + hc_{0} \frac{\rho_{0}}{\rho_{i}} \sum_{j} \alpha_{ij} \pi_{ij} \nabla_{i} W_{ij} V_{j}, \\ \frac{D\boldsymbol{r}_{i}}{Dt} = \boldsymbol{u}_{i}, \qquad p_{i} = c_{0}^{2} (\rho_{i} - \rho_{0}). \end{cases}$$

$$\delta_{ij} = 2 \frac{\delta_i \delta_j}{\delta_i + \delta_j}, \qquad \delta_i = \frac{v_i^{\delta}}{c_0 h}, \qquad v_i^{\delta} = (C_{\delta} l_{LES})^2 ||\mathbb{D}||_i$$

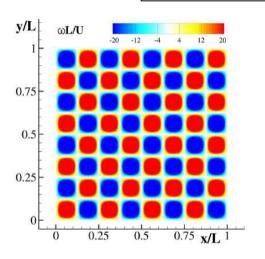
The viscous term in the momentum equation and the diffusive term in the continuity equation are interpreted as closures in the **LES framework** 

### => dynamic choice of coefficients using the velocity deformation tensor

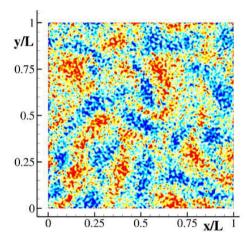
$$\begin{cases} \frac{D\rho_{i}}{Dt} = -\rho_{i} \sum_{j} (\boldsymbol{u}_{j} - \boldsymbol{u}_{i}) \cdot \nabla_{i} W_{ij} V_{j} + hc_{0} \sum_{j} \delta_{ij} \mathcal{D}_{ij} \cdot \nabla_{i} W_{ij} V_{j}, \\ \frac{D\boldsymbol{u}_{i}}{Dt} = \boldsymbol{g}_{i} - \frac{1}{\rho_{i}} \sum_{j} \left( p_{i} + p_{j} \right) \nabla_{i} W_{ij} V_{j} + hc_{0} \frac{\rho_{0}}{\rho_{i}} \sum_{j} \alpha_{ij} \pi_{ij} \nabla_{i} W_{ij} V_{j}, \\ \frac{D\boldsymbol{r}_{i}}{Dt} = \boldsymbol{u}_{i}, \qquad p_{i} = c_{0}^{2} (\rho_{i} - \rho_{0}). \end{cases}$$

$$\alpha_{ij} = \alpha + 2 \frac{\alpha_i \alpha_j}{\alpha_i + \alpha_j}, \quad \alpha = \frac{K \mu}{c_0 h \rho_0}, \qquad \alpha_i = \frac{K v_i^T}{c_0 h}. \qquad v_i^T = (C_s l_{LES})^2 ||\mathbb{D}||_i,$$

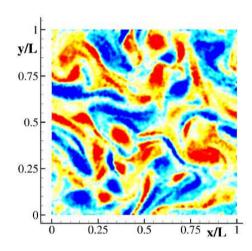
Two-dimensional freely-decaying turbulence:  $Re_i = 125,000$ 



Initial vorticity field (2D vortex pattern)



DNS by using SPH (insufficient resolution)



LES-SPH
(same resolution,
correct modelling of
large vortex structures)

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# Thank you for your attention!