

HEIG-VD / Hes-so

Magnetocaloric elements with thermoelectric switches:

Magneto-Thermodynamics of Layered Beds

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A personal statement

We are not competitive enough with present developments (good efficiency is possible, but too high cost)!

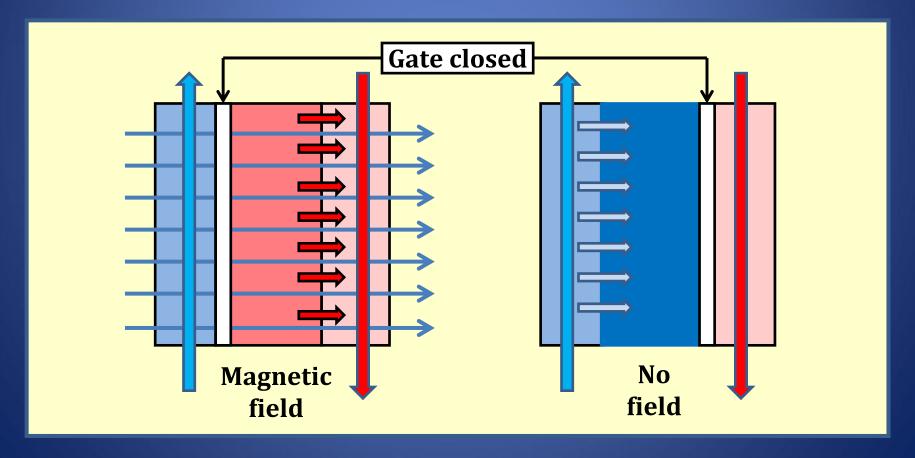
Demand:

5 x higher magnetocaloric effect of materials or

5 x higher frequency of the machines

Thermal switch technology

Advantage: Constant fluid flows with alternating cold/heat inputs (no carry over leckage, no fluid switches)

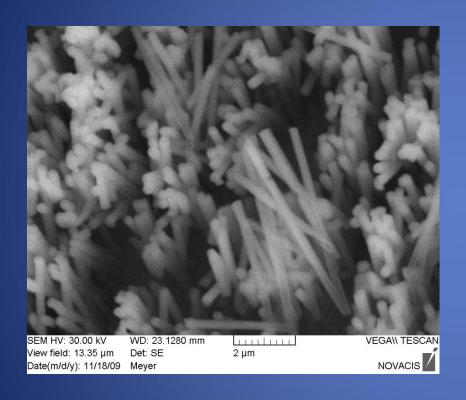


Three basic elements

- 1) Thermoelectric switches
- 2) Micro channel heat exchangers
- 3) Magneto caloric layered bed (Delft Days 2011)

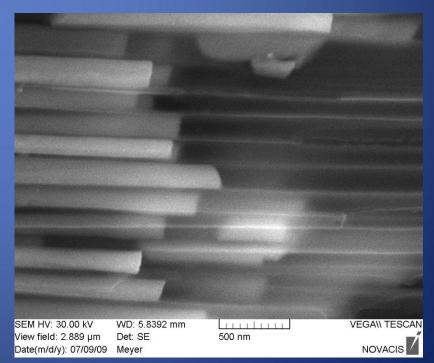
Full presentation 1) to 3):
THERMAG V
Grenoble/Annecy
17-21 September 2012

Thermoelectric switches



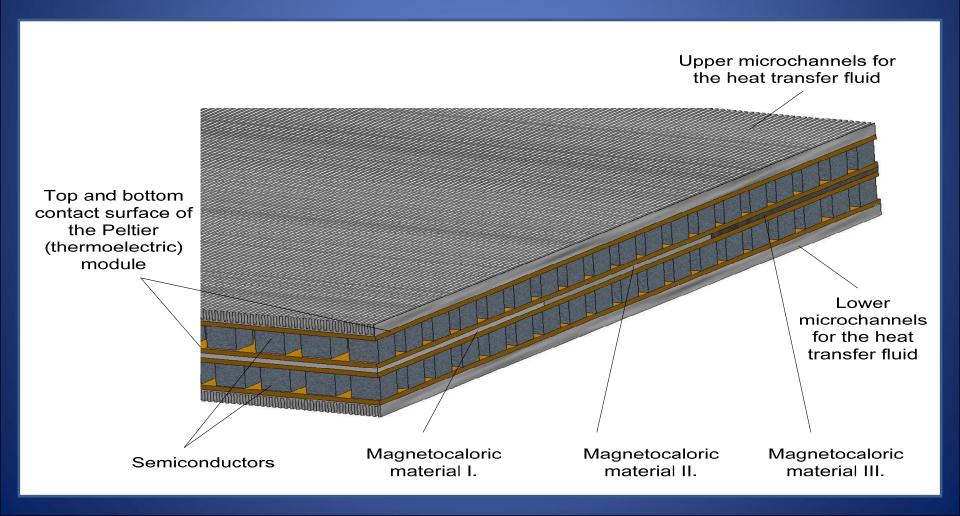
SME: Dr. Anne-Gabrielle Pawlowski, MNT

Characteristic diameter of the Ni wires is 200 nm

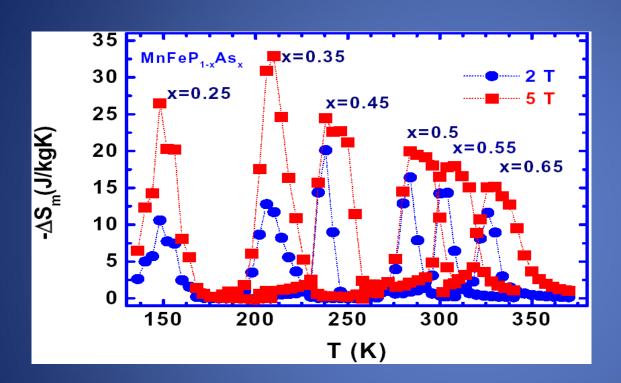


Micro channel heat exchangers

Kitanovski and Egolf, Int. J. Refr. 33 (3), 449-464:



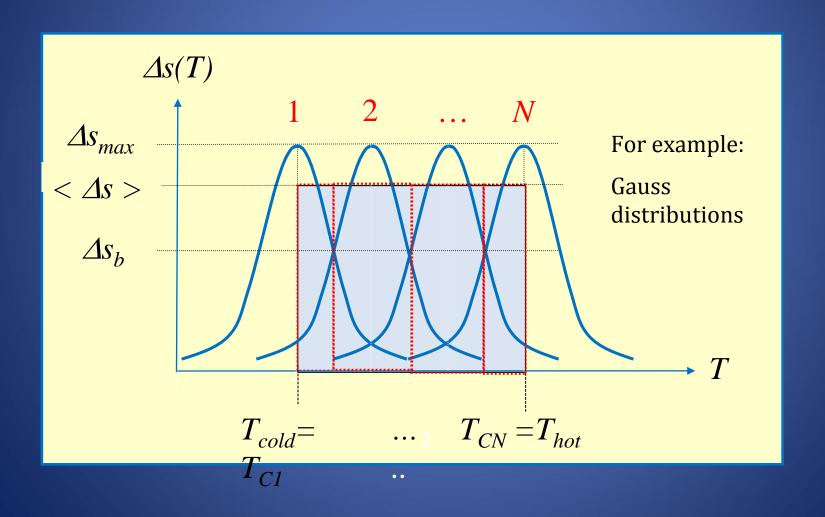
Varying Curie temperature



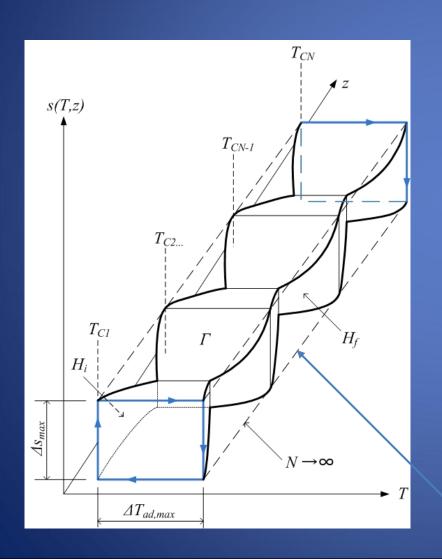
A manganese based magneto caloric material showing a giant magneto caloric effect.

The alteration of the stoechiometric ratio of phosphor and arsenic leads to a shift of the Curie temperature (PhD O. Tegus, Univ. Amsterdam, with permission by Ekkes Brück).

Model of magneto caloric layered bed



The *T-s-z* diagram



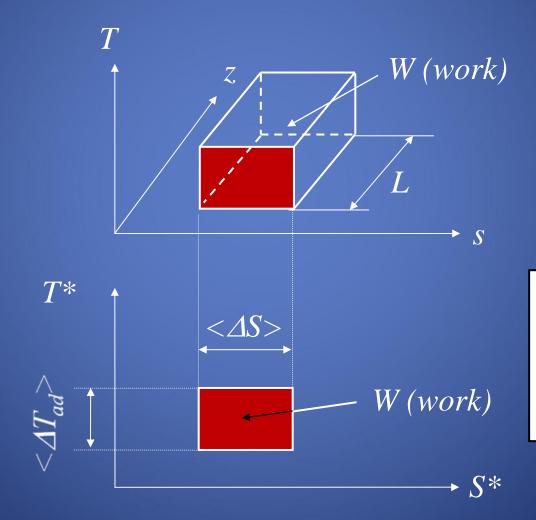
Here a thermodynamic cycle of a magnetic heat pump, respectively refrigerator is presented. A layered bed is described by a body with a certain number of contractions and enlargements. The largest cross sections are obtained at the Curie points.

Maximal (or average) value

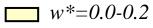
Is the T-S diagram appropriate?

Case: A

T=const *s*=const



In this simplest case:
Yes!



$$w*=0.2-0.4$$

$$w*=0.4-0.6$$

$$w*=0.6-0.8$$

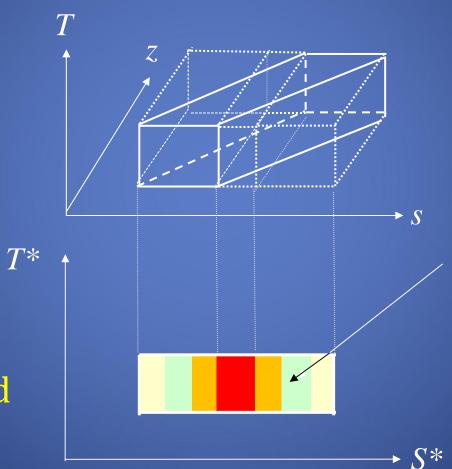
$$w*=0.8-1.0$$

Is the T-S diagram appropriate?



T=const *s*≠const

Integration and not projection!



In this case:
No!

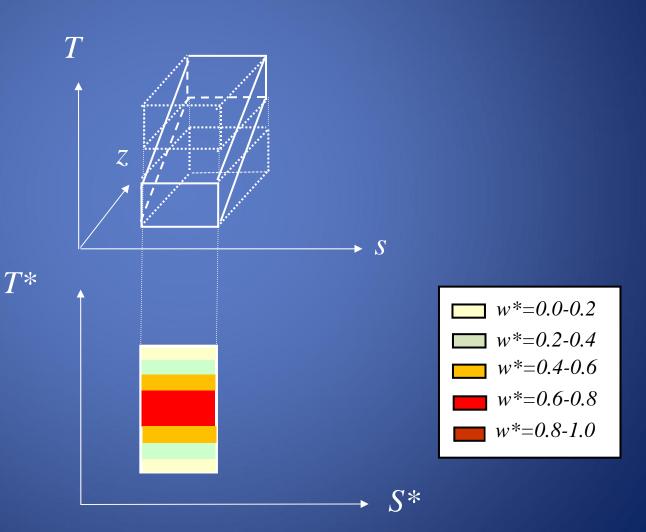
Work W is larger! Weights w*:

- $w^*=0.0-0.2$
- w*=0.2-0.4
- $w^*=0.4-0.6$
- w*=0.6-0.8
- w*=0.8-1.0

Proposal: T*-S* diagram

Case C:

 $T \neq \text{const}$ s = const

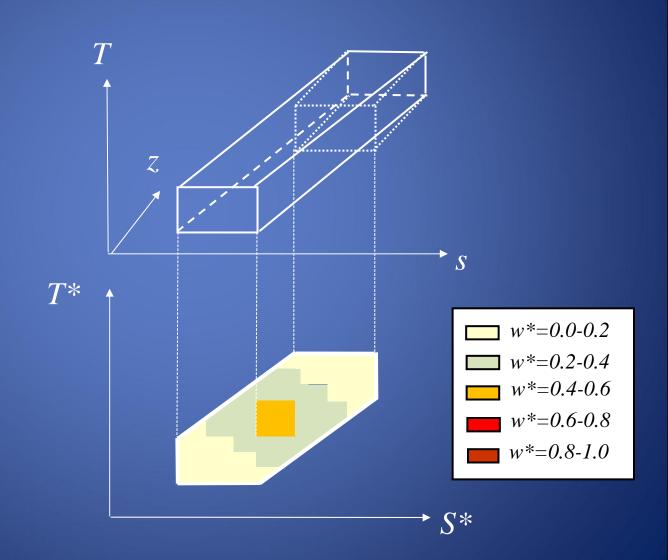


Isoline weight distribution

Case D:

 $T \neq \text{const}$ $s \neq \text{const}$

T(z) is usually even not linear!



Isoline weight distribution

$$W = \iint_{\partial \Gamma} T \, dS = \iint_{\partial \Gamma^*} w^* (S^*, T^*) T^* \, dS^*, \qquad S^* \leq S, \forall S$$

 $\partial\Gamma*$ is the enclosed domain in the projected T-s-z diagram T^* - S^* , where the weight distribution $w^*(T^*, S^*)$ is applied.

Thermodynamics for a single layer

The work performed*:

$$W = A \int_{0}^{L} \Delta T_{ad}(z) \cdot \Delta s(z) dz$$

Full correlation:

$$W = V < \Delta T_{ad} > \cdot < \Delta s >$$

The heat *Q* (heat pump application):

$$Q = A \int_{0}^{L} \left[T(z) + \Delta T_{ad}(z) \right] \Delta s(z) dz$$

^{*} Symmetry perpendicular to downstream direction!

Thermodynamics for a single layer

This is identical to:

$$Q = V < T > \cdot < \Delta s > + W$$

Taylor approximation* at the Curie temperature:

$$T(z) = T_{in} + \frac{dT}{ds} \bigg|_{T_C} \left\{ s [H_i, T(z)] - s [H_i, T_{in}] \right\} + O\left\langle \left\{ s [H_i, T(z)] - s [H_i, T_{in}] \right\}^2 \right\rangle$$

With:

$$< s[H_i, T(z)] - s[H_i, T_{in}] > = \frac{s[H_i, T(L)] - s[H_i, T(0)]}{2} = \frac{< \Delta s > 1}{2}$$

^{*} Approximation is possible because of many thin layers!

Thermodynamics for a single layer

This is identical to:

$$Q = V \left[\langle T_{in} \rangle + \frac{\beta}{2} \langle \Delta s(z) \rangle \right] \langle \Delta s(z) \rangle + W, \qquad \beta = \frac{dT}{ds} \Big|_{T_C}$$

Now the *COP* of a single layer of a heat pump is:

$$< COP > = \frac{< Q >}{< W >} = \frac{< T_{in} > + \frac{\beta}{2} < \Delta s > + < \Delta T_{ad} >}{< \Delta T_{ad} >} = \frac{< T_{in} >}{< \Delta T_{ad} >} + \frac{\beta}{2} \frac{< \Delta s >}{< \Delta T_{ad} >} + 1$$

Thermodynamics for multiple layers

A layered bed with N layers (special case) leads to*:

$$< T_{out} > - < T_{in} > = N < \Delta T_{ad} >$$

Similar as before, one obtains:

$$< COP > = \frac{V_N}{V} \left(\frac{\langle T_{in} \rangle}{\langle \Delta T_{ad} \rangle} + \frac{\beta}{2} \frac{\langle \Delta s \rangle}{\langle \Delta T_{ad} \rangle} \right) + \frac{N V_N}{V}$$

In the case of a linear T(z) dependence:

$$V_N = \frac{V}{N} \qquad \Rightarrow \qquad \langle COP \rangle = \frac{1}{N} \left(\frac{\langle T_{in} \rangle}{\langle \Delta T_{ad} \rangle} + \frac{\beta}{2} \frac{\langle \Delta s \rangle}{\langle \Delta T_{ad} \rangle} \right) + 1$$

^{*} By adapting Δs_h one can obtain an integer number N!

Thermodynamics for multiple layered bed

In the case of an infinite number of layers and a finite ΔT_{ad} :

$$< COP > = \frac{1}{N} \left(\frac{\langle T_{in} \rangle}{\langle \Delta T_{ad} \rangle} + \frac{\beta}{2} \frac{\langle \Delta s \rangle}{\langle \Delta T_{ad} \rangle} \right) + 1, \qquad \lim_{N \to \infty} < COP > = 1$$

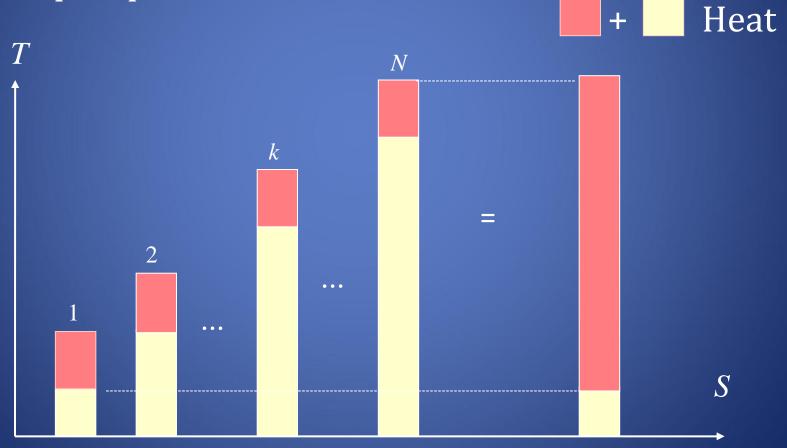
the heat pump degenerates to an electric heater!

In the special case that β =0:

$$<\!COP\!> = \frac{<\!T_{in}\!> + N <\!\Delta T_{ad}\!>}{N <\!\Delta T_{ad}\!>} = \frac{<\!T_{out}\!>}{<\!T_{out}\!> - <\!T_{in}\!>} = <\!COP_{Carnot}\!>$$

Thermodynamics for multiple layered bed

The simple special case:



Work

Conclusions and outlook

- 1) A generalized T^* - s^* diagram is proposed containing a weight distribution $w^*(T^*,S^*)$
- 2) N layers of a layered bed act as a cascade of N smaller refrigerators, respectively heat pumps
- 3) The layered bed technique doesn't lead to lower efficiency (*COP*)
- 4) The layered bed technique leads to larger magnet assemblies, volume and prize
- 5) We can counterbalance this with stronger MCE or higher frequencies *f* of the thermodynamic process