



Investigating the validity of the fundamental derivative in the equilibrium and non-equilibrium two-phase expansion of MM

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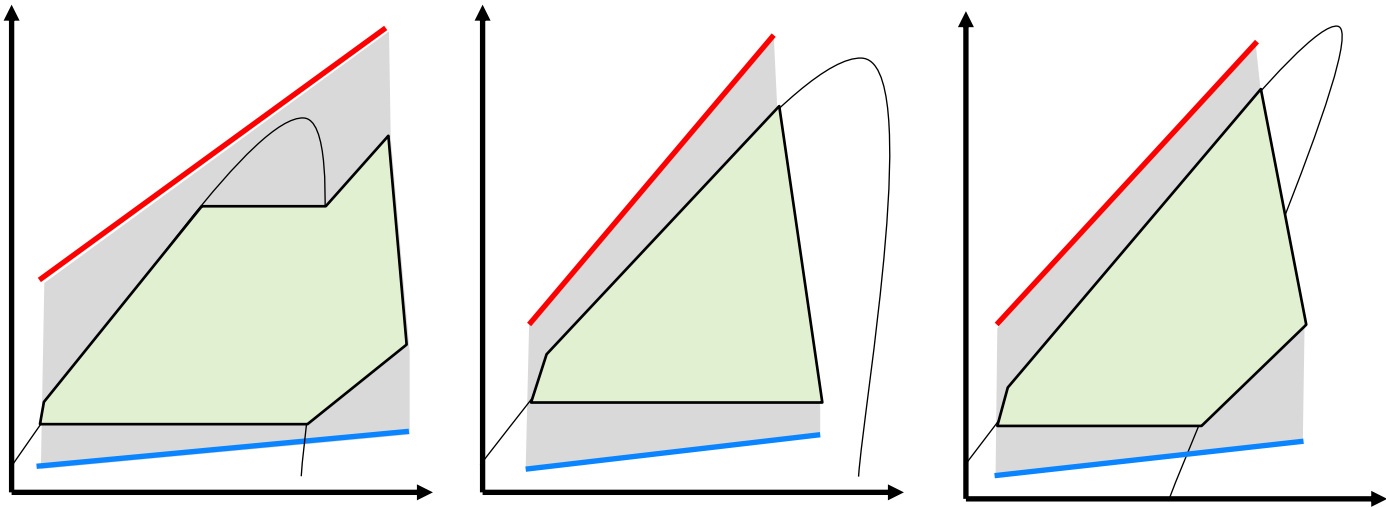
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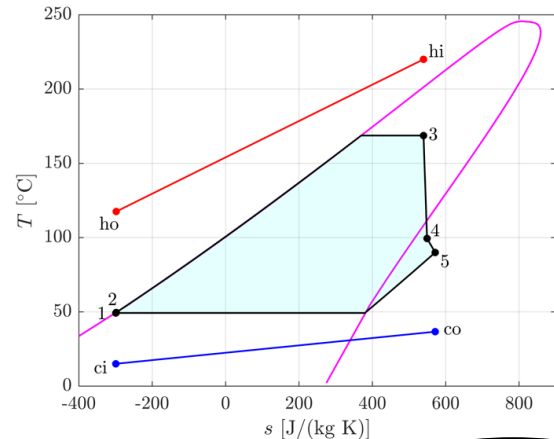
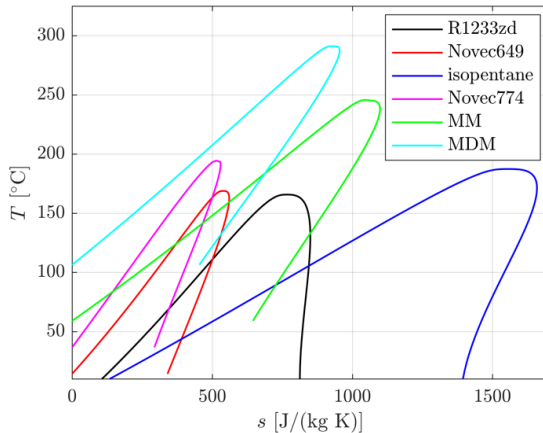
**Royal Academy
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The motivation for two-phase expansion



Characteristics of a two-phase ORC turbine



molecularly complex working fluid

low turbine inlet vapour quality

high turbine inlet pressure

low degree of reaction turbine → high stator expansion ratio

transition for low vapour quality to superheated vapour in stator

molecular complexity,
supersonic flow,
high pressure

two-phase ORC

two-phase flow,
non-equilibrium flow

Modelling overview

$$\Gamma = 1 + \frac{\rho}{a} \left(\frac{\partial a}{\partial \rho} \right)_s$$

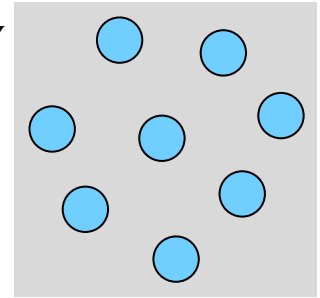
Require a definition for the speed of sound

Speed of sound will depend on:

- thermal interaction between phases
- mechanical interaction between phases

$$u_V, \rho_V, T_V$$

$$u_L, \rho_L, T_L, D$$



| | Momentum equilibrium | Momentum non-equilibrium |
|-------------------------|-------------------------------|----------------------------------|
| Thermal equilibrium | $u_L = u_V$ $T_L = T_V$ | $u_L \neq u_V$ $T_L = T_V$ |
| Thermal non-equilibrium | $u_L = u_V$ $T_L \neq T_V$ | $u_L \neq u_V$ $T_L \neq T_V$ |

homogeneous flow

Homogeneous modelling

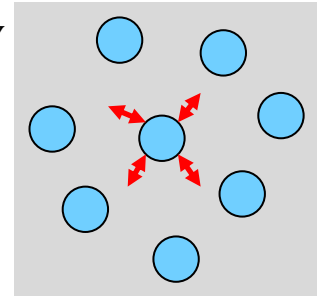
Assumptions:

- well mixed
- very small particle diameter
- negligible surface tension effects

$$p_L = p_V$$

$$u_L = u_V$$

$$u_V, \rho_V, T_V$$
$$u_L, \rho_L, T_L, D$$



Two extreme cases for heat exchange between phases:

- $\rightarrow \infty$ $T_L = T_V = T_{\text{sat}}$ \longrightarrow **thermal equilibrium**
- $\rightarrow 0$ insulated \longrightarrow **frozen thermal states**

Homogeneous equilibrium modelling

Speed of sound with phase change (Brennen, 2005):

$$\frac{1}{\rho a^2} = \alpha g_V + (1 - \alpha) g_L$$

where:

$$g_i = \frac{1}{\rho_i} \left(\frac{\partial \rho_i}{\partial p} \right)_e - \frac{1}{h_{LV}} \left(\frac{1}{\rho_V} - \frac{1}{\rho_L} \right) \left(1 - \rho_i \left(\frac{\partial h_i}{\partial p} \right)_e \right)$$

α : vapour volume fraction

e : phase derivative

h_{LV} : latent heat of vapourisation

Homogeneous frozen-state modelling

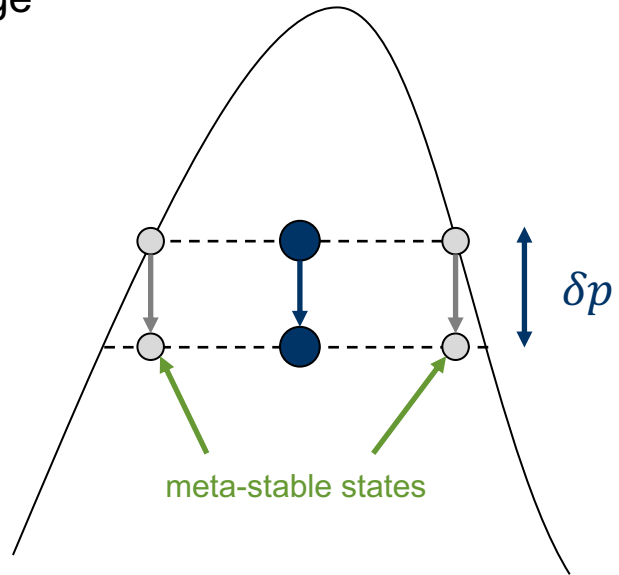
Speed of sound without phase change
(Brennen, 2005):

$$\frac{1}{\rho a^2} = \frac{\alpha}{\rho_V a_V^2} + \frac{(1 - \alpha)}{\rho_L a_L^2}$$

where:

$$a_i = \sqrt{\left(\frac{\partial p}{\partial \rho_i}\right)_s}$$

α : vapour volume fraction
 s : entropy

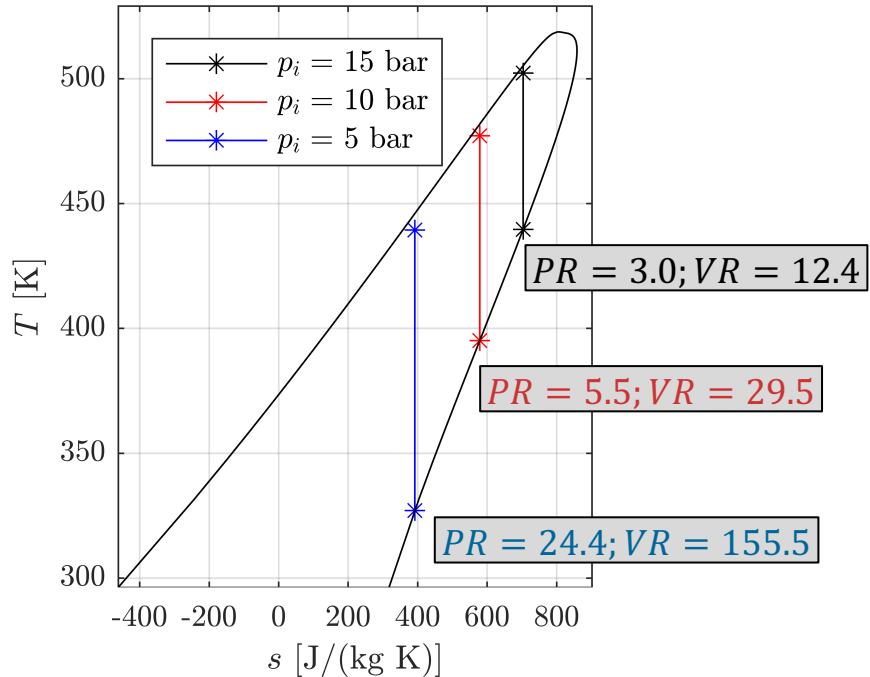


Case study

Working fluid:
MM

Inlet pressures:
5, 10, 15 bar

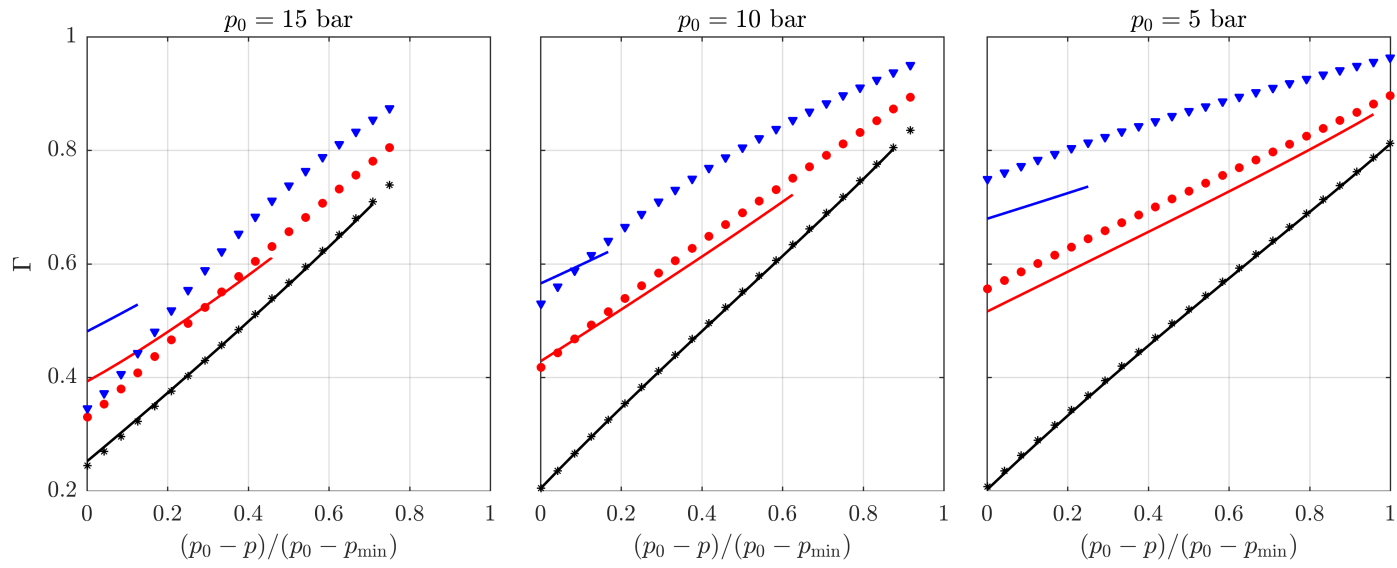
Inlet vapour qualities:
0.1, 0.5, 0.9



PR : pressure ratio
 VR : volumetric expansion ratio

Fundamental derivative comparison

— $eq : X_0 = 0.1$ * $fr : X_0 = 0.1$ — $eq : X_0 = 0.5$ • $fr : X_0 = 0.5$ — $eq : X_0 = 0.9$ ▽ $fr : X_0 = 0.9$



Conclusions and future works

Two-phase expansion promising candidate for ORC systems

Preliminary investigation of NICFD effects within the two-phase expansion of MM under relevant ORC operating conditions

Expressions for the speed of sound defined and fundamental derivative evaluated for homogeneous thermal equilibrium and frozen thermal states

From reservoir pressures of 5, 10 and 15 bar with reservoir vapour qualities of 0.1, 0.5 and 0.9 expansion remains within a region where $0 < \Gamma < 1$

Deviation in Γ under the frozen state and thermal equilibrium assumptions increased at higher vapour qualities and most significant at high reservoir pressures

Assumption of a homogeneous two-phase mixture is likely an oversimplification, and further investigations are required



Thank you for listening

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