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# DESIGN OF A CLOSED LOOP SCO<sub>2</sub> WIND TUNNEL: NUMERICAL MODELLING OF NON-EQUILIBRIUM CONDENSATION IN A CONVERGING-DIVERGING NOZZLE

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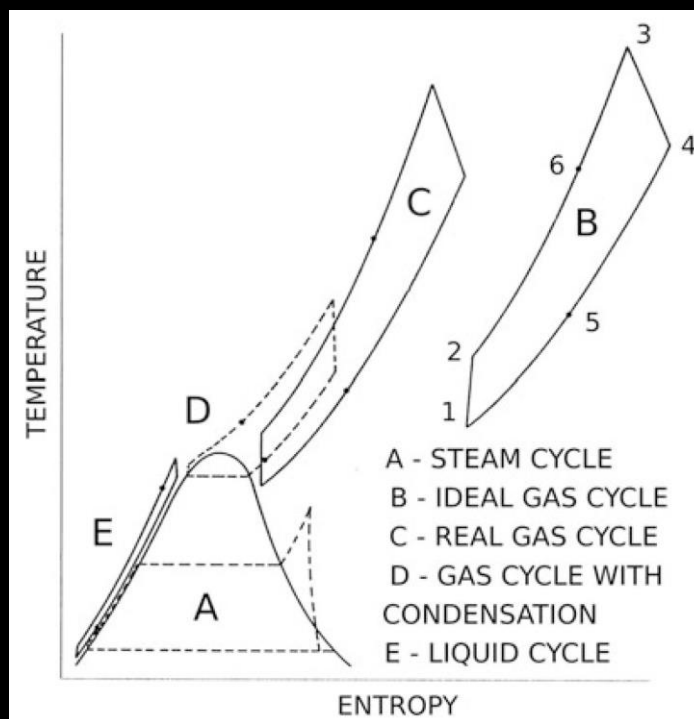
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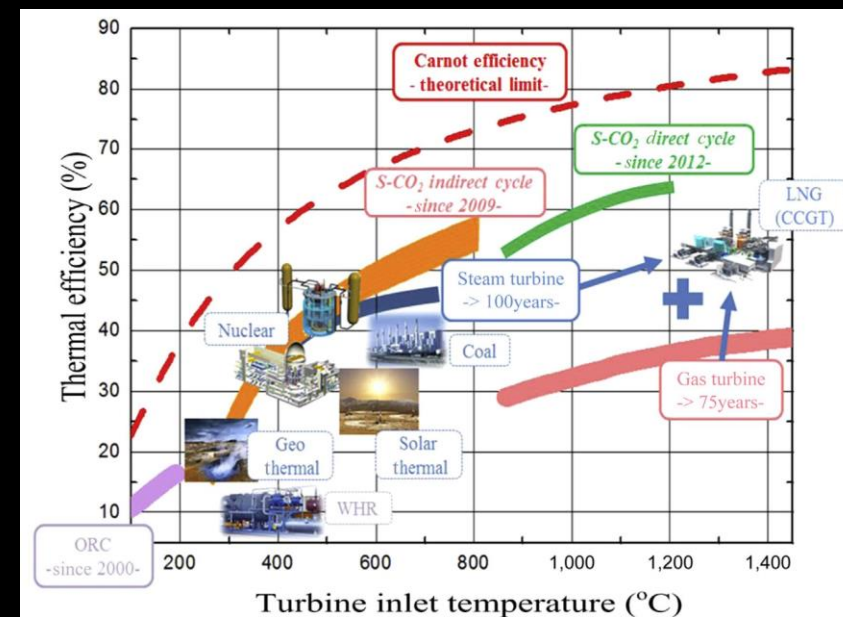
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# S-CO<sub>2</sub> APPLICATIONS AND POWER CYCLES

- sCO<sub>2</sub> is compressed in the near-incompressible region (cycles C and D)
- Compactness and high efficiencies
- Suitable for different heat sources ( $T_{cr} = 31^{\circ}\text{C}$ )
- Higher TIT achievable compared to steam cycles



(Invernizzi, 2013)

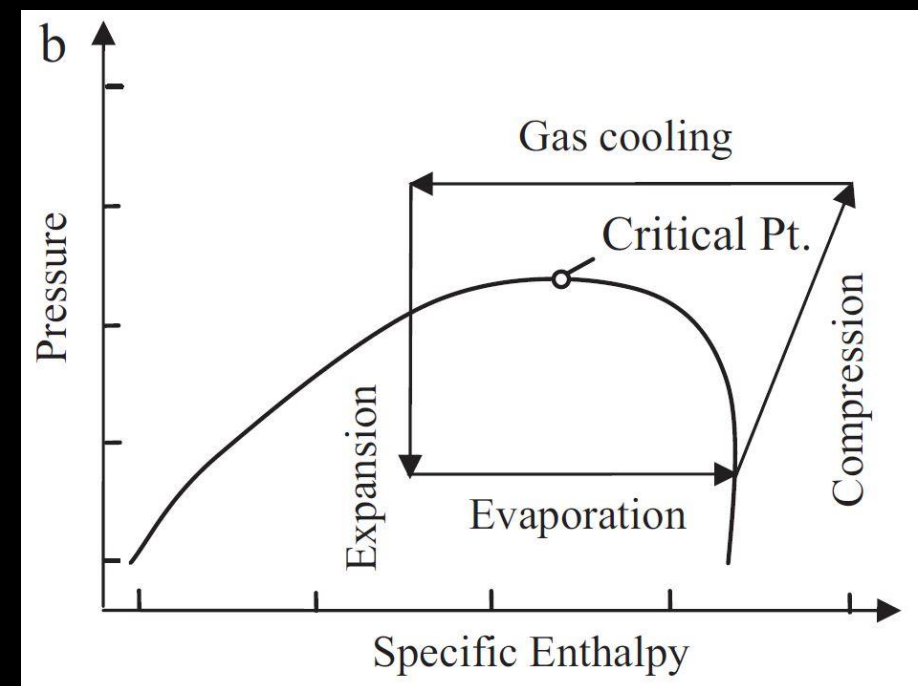


(Ahn et Al., 2015)

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# TRANSCRITICAL REFRIGERATION CYCLE

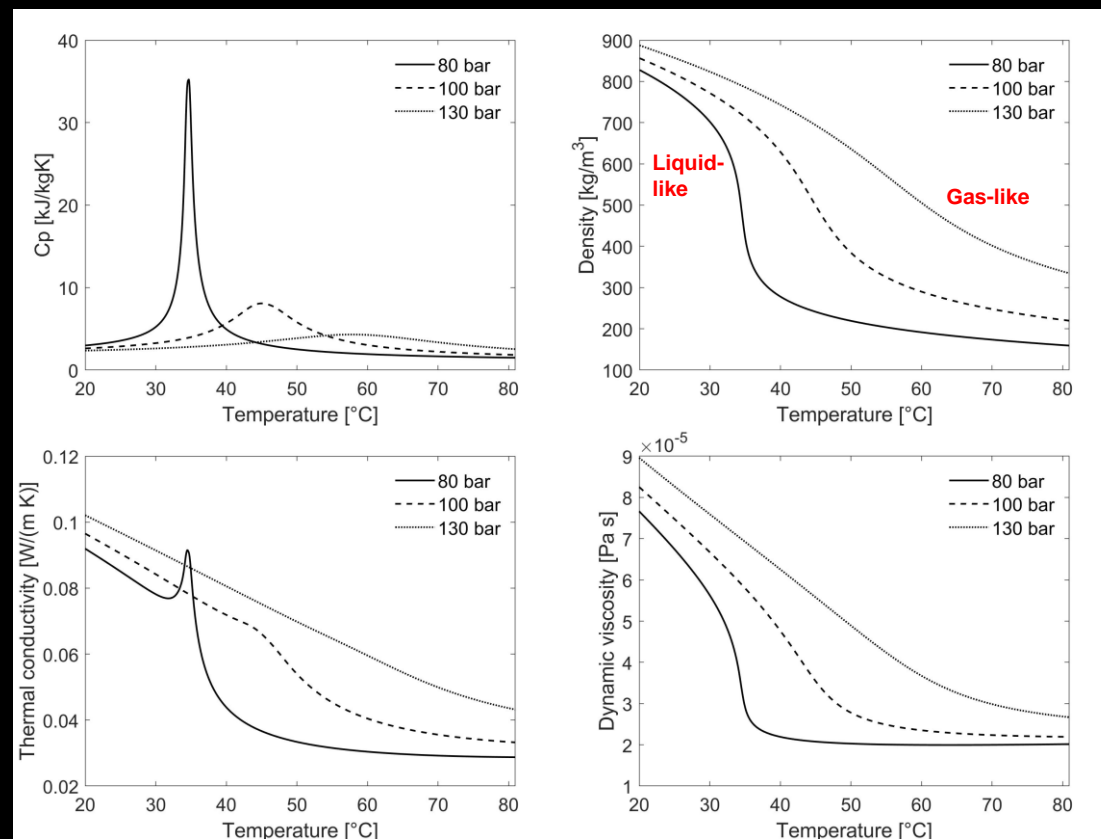
- » CO<sub>2</sub> is safe (not toxic, flammable or corrosive) and economic
- » Alternative to ozone-depleting and global-warming refrigerants
- » Possibility of operating with heat rejection temperatures close to the critical point with pressures up to 130 bar
- » Technology becoming standardized, costs are strongly decreasing



(Austin et Al., 2011)

# THERMOPHYSICAL PROPERTIES

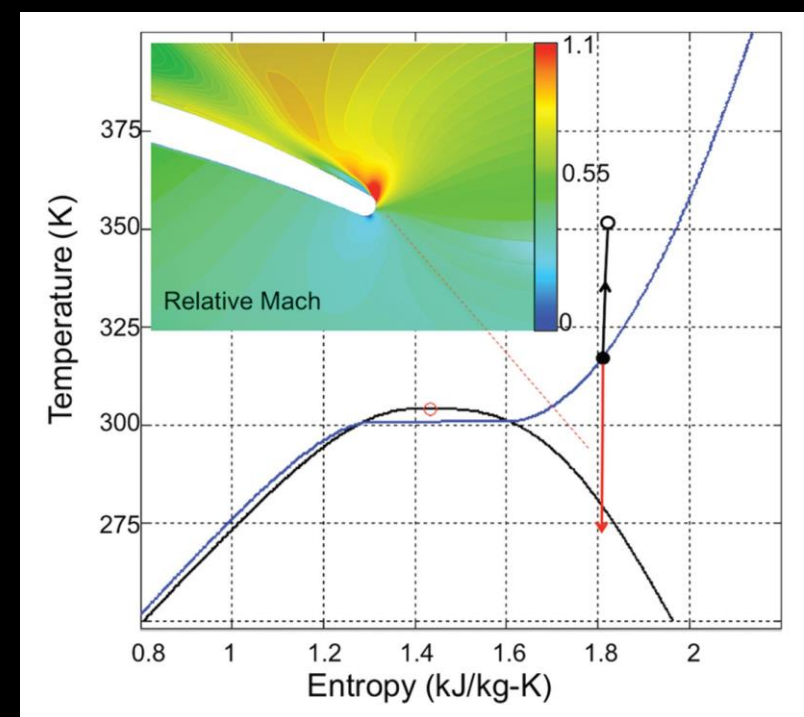
- » Compressibility factor:  $Z = \frac{P}{\rho RT}$
- » Real-gas behaviour of the fluid in the supercritical region ( $Z = 0.2 \div 0.5$ )
- » Sharp variations of the fluid properties in the region near the critical point (31 °C, 73.8 bar)
- » Transition from liquid-like to gas-like behaviour crossing the pseudo-boiling temperature at supercritical pressures



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# POSSIBLE CONDENSATION IN COMPRESSORS

- Flow acceleration on the suction side of the compressor blade may cause the nucleation of liquid droplets
- Condensation would affect the performance of the machine
- Lettieri et al. defined a criterion to determine a limit for condensation-free inlet conditions of compressors

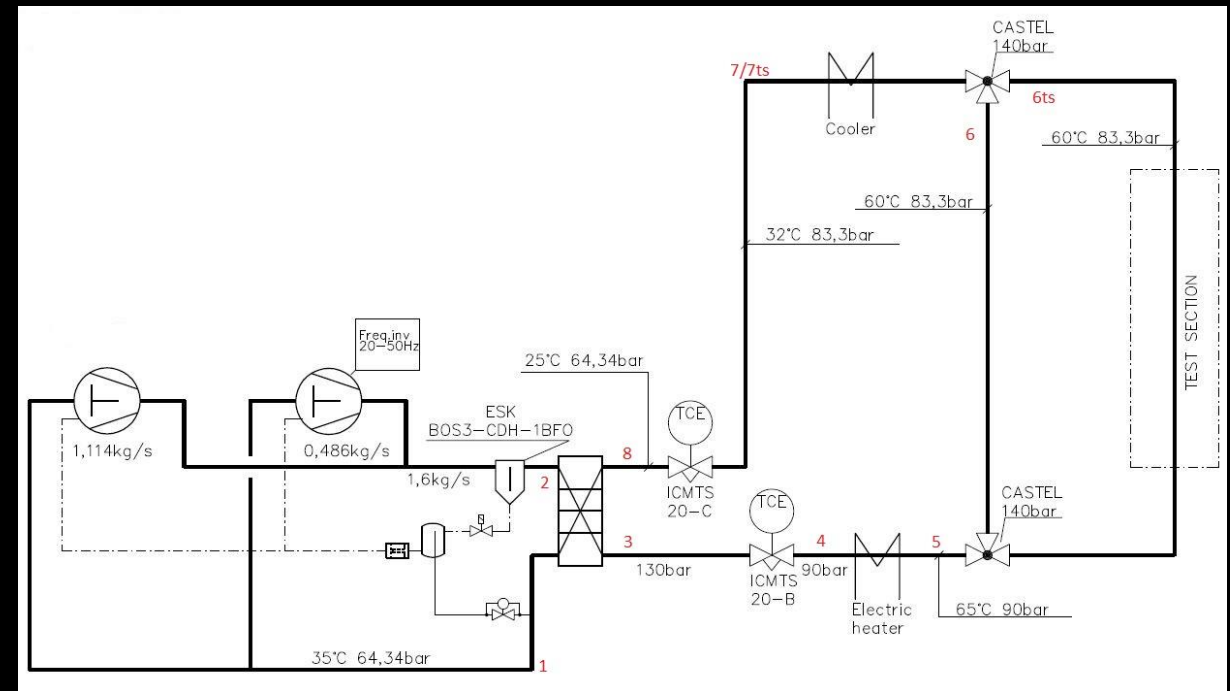
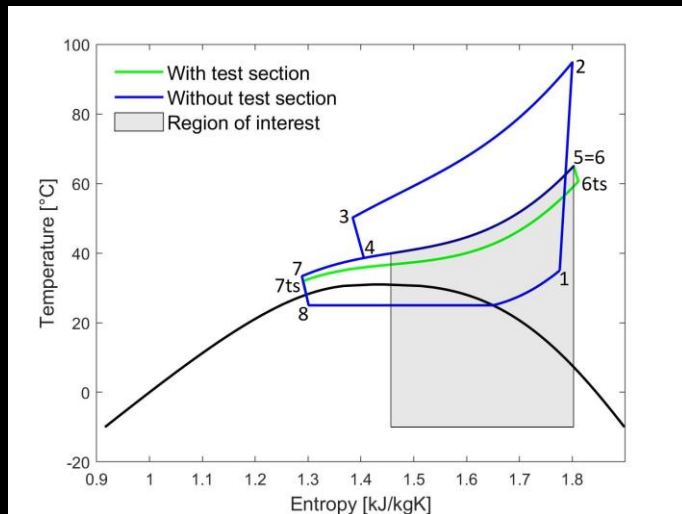


(Baltadjiev et Al, 2015)

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# THERMODYNAMIC CYCLE AND LAYOUT

- Constraints on total required power (~500 kW) and dimensions.
- Research interests:
  - Heat transfer across the pseudoboiling line
  - Expansion from supercritical condition
  - Non-equilibrium condensation



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# SUPERSONIC TEST SECTION

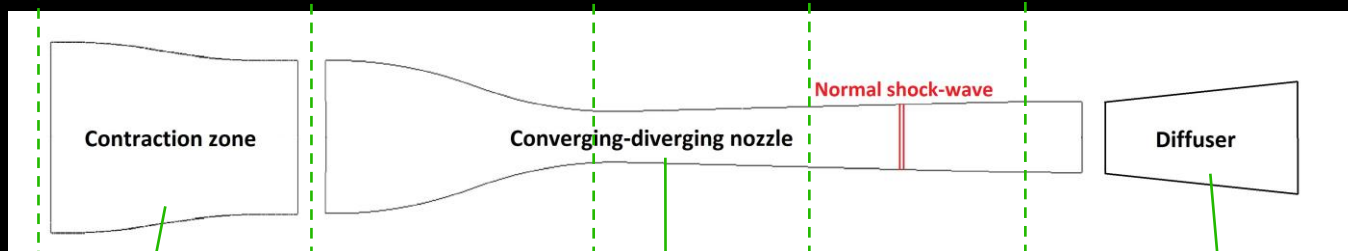
$P_0 = 90 \text{ bar}$   
 $T_0 = 65 \text{ }^\circ\text{C}$

$M = 0.2$

$M = 1$

$M > 1$

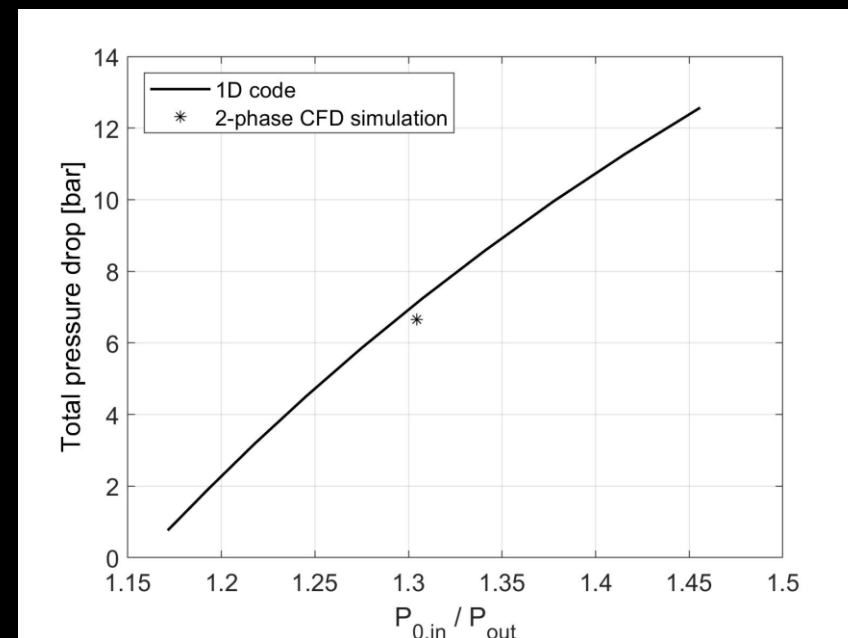
$M < 1$



Transition from circular to rectangular cross-section

Supersonic expansion and condensation

Recovery of the kinetic energy



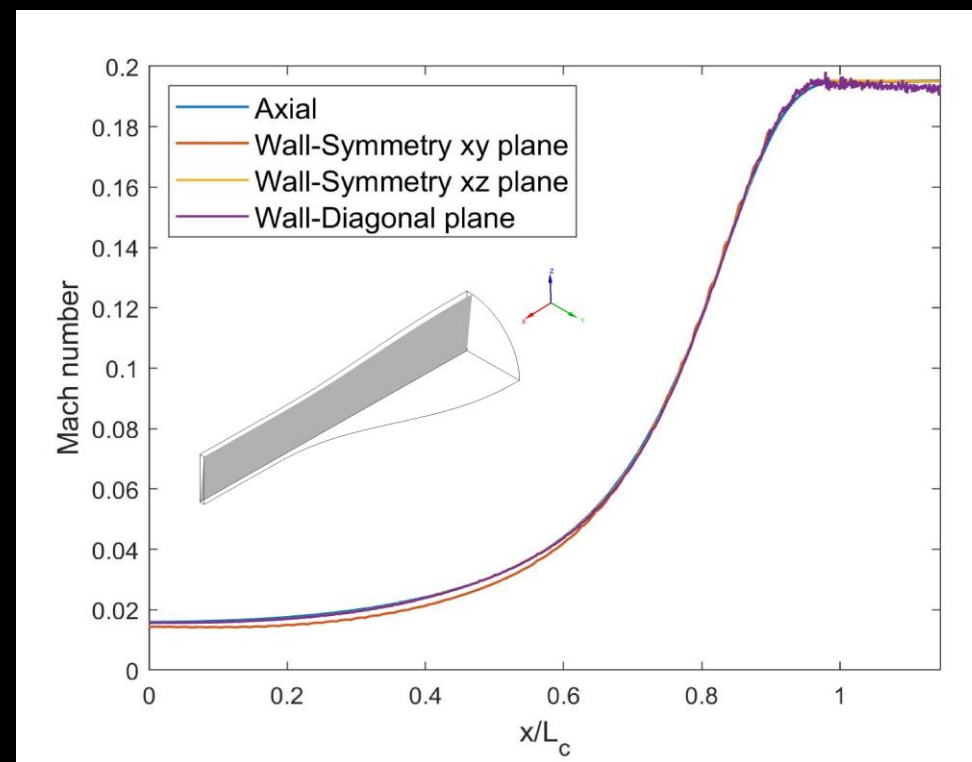


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# CONTRACTION ZONE: CFD RESULTS

- Real-gas CFD simulation carried out in Ansys Fluent
- Unstructured mesh with ICEM CFD
- Total pressure loss coefficient:

$$Y = \frac{P_{0,in} - P_{0,out}}{P_{0,out} - P_{out}} = \begin{cases} 0.0004 & \text{Inviscid} \\ 0.0348 & \text{Viscous} \end{cases}$$



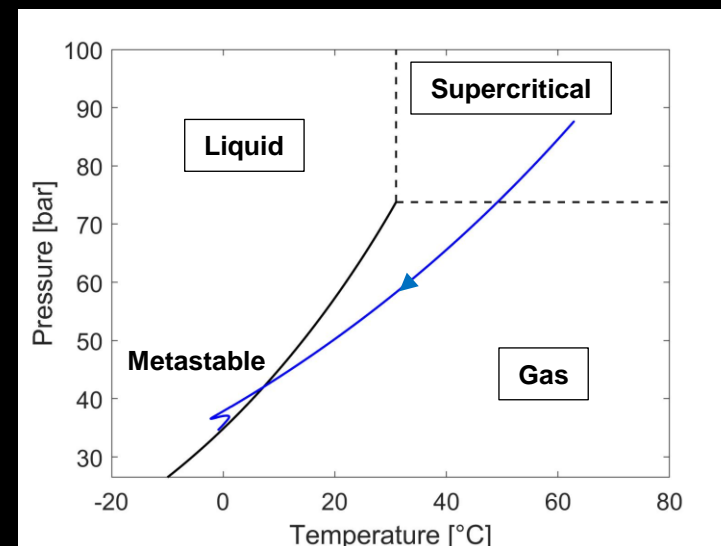
# NON-EQUILIBRIUM CONDENSATION MODEL

Droplets nucleation rate: 
$$J = \frac{1}{1 + \theta} \frac{\rho_g^2}{\rho_l} \sqrt{\frac{2\sigma}{\pi M^3}} \cdot \exp\left(-\frac{4\pi r^{*2} \sigma}{3k_B T_g}\right)$$

Critical radius: 
$$r^* = \frac{2\sigma}{\rho_l R T_g \int_{P_s}^P \frac{Z}{P} dP} = \frac{2\sigma}{\rho_l R T_g [\ln S + A(P_s) \cdot P_s (S - 1)]}$$

Droplet growth rate model: 
$$\frac{dr}{dt} = \frac{k_g}{r \rho_l \left[ \frac{1}{1 + 4Kn} + 3.78(1 - \nu) \frac{Kn}{Pr_g} \right]} \left( \frac{T_l - T_g}{L} \right)$$

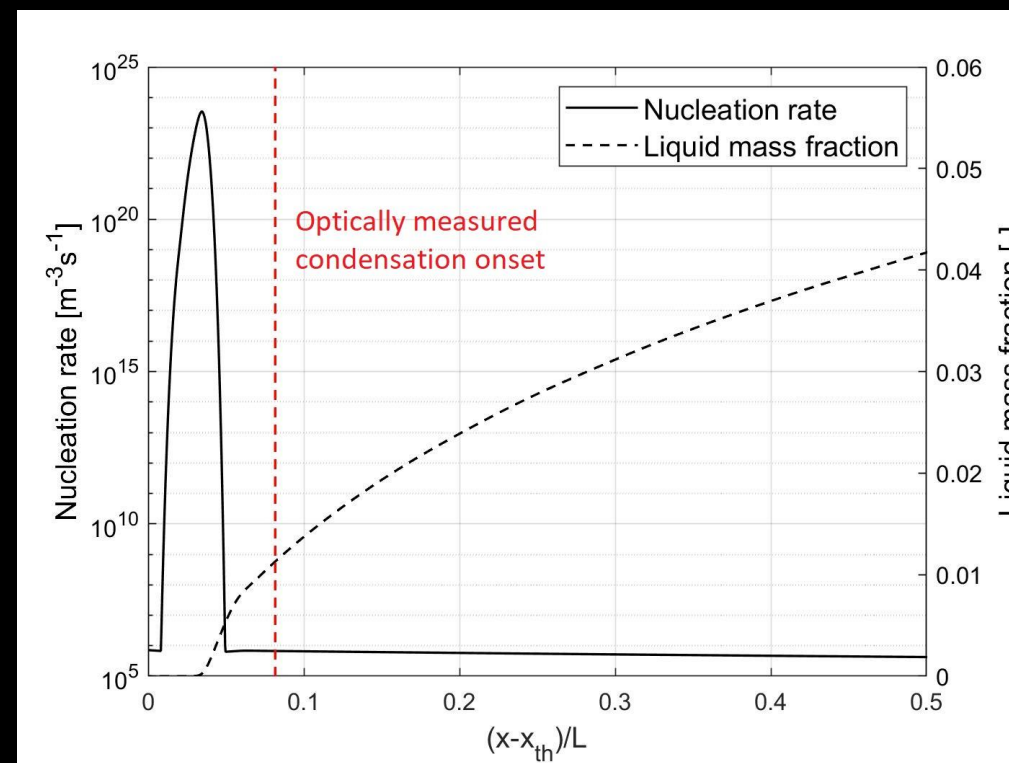
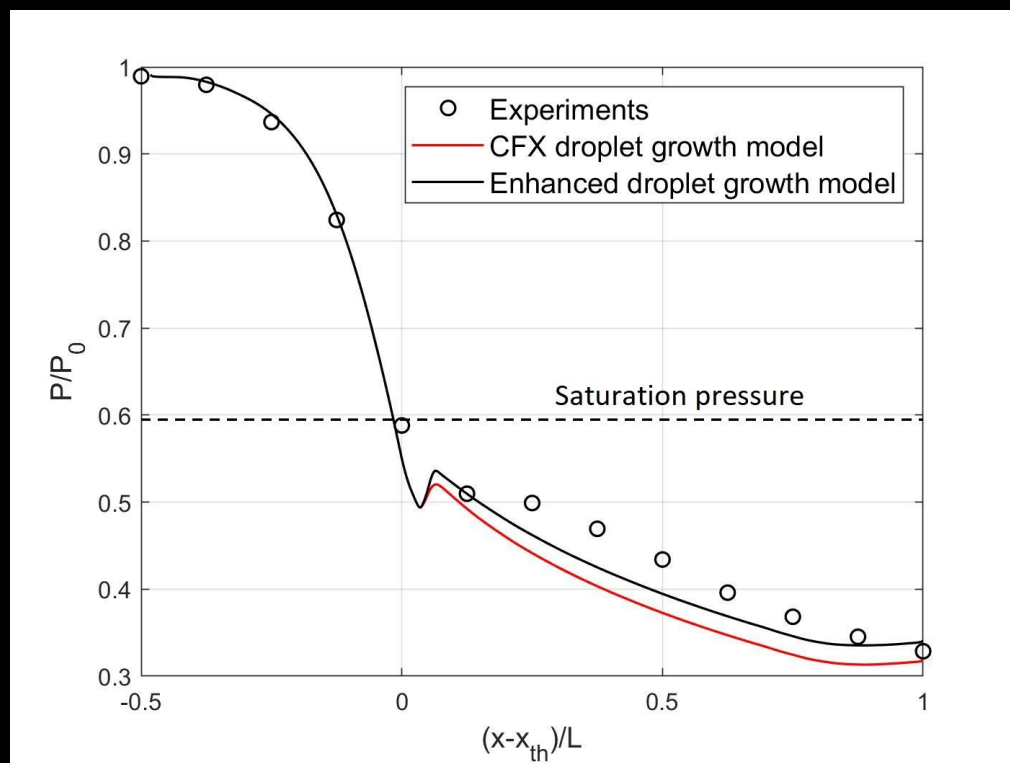
$$T_l = T_s(P) - [T_s(P) - T_g] \frac{r^*}{r}$$



- $\theta$  Non-isothermal correction term
- $\sigma$  Surface tension
- $M$  Molecular mass
- $k_B$  Boltzmann constant
- $S$  Supersaturation ratio
- $\nu$  Young modification parameter
- $Kn$  Knudsen number
- $Pr$  Prandtl number

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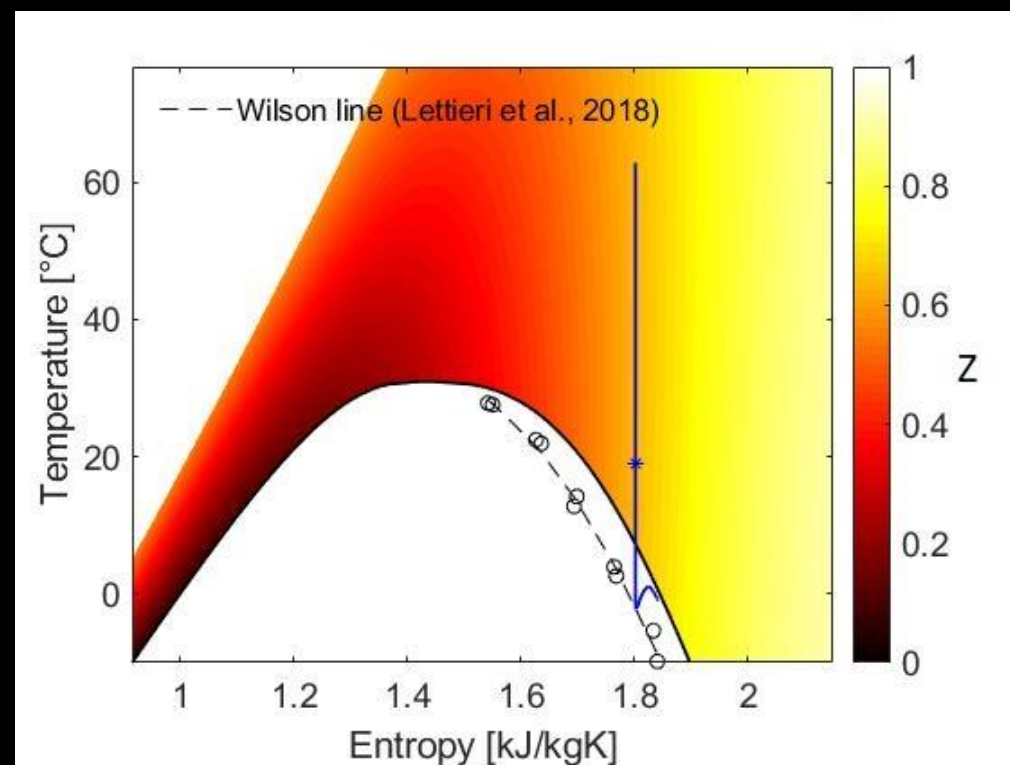
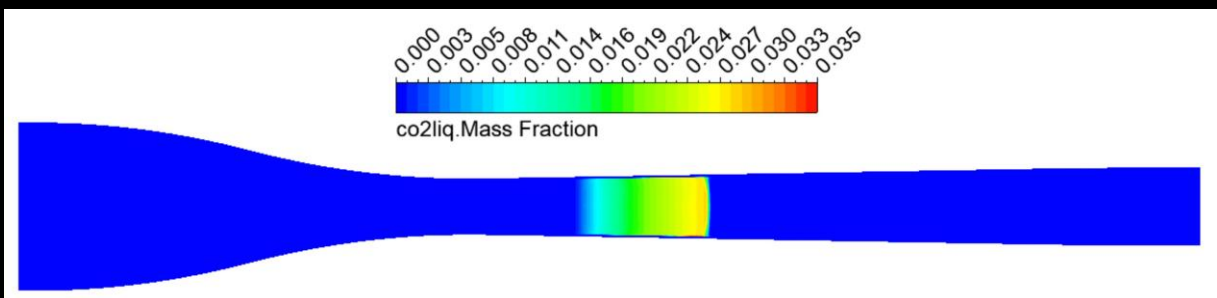
# VALIDATION OF THE CONDENSATION MODEL



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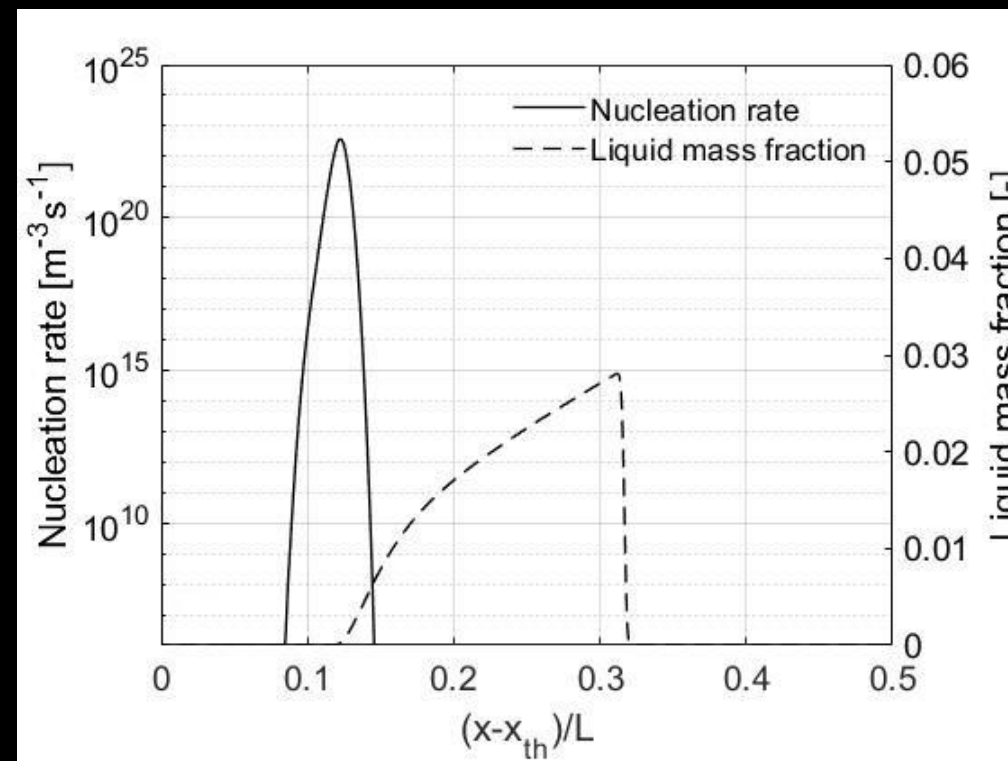
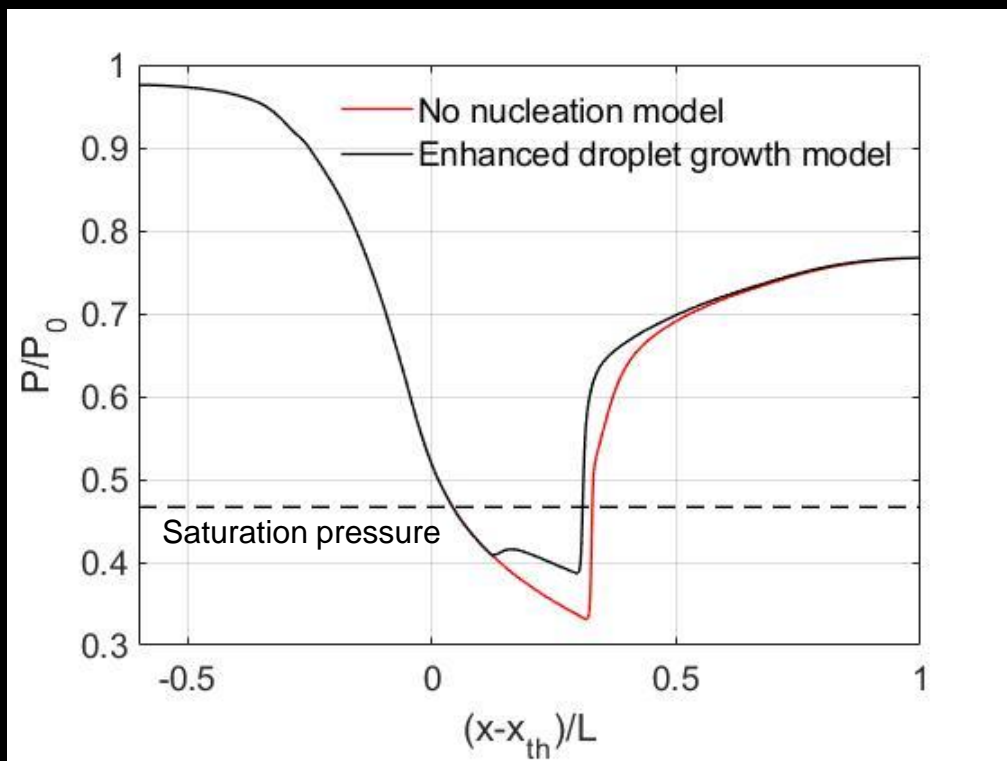
# DESIGNED NOZZLE: EXPANSION AND CONDENSATION

- Expansion rate:  $\dot{p} = -\frac{w}{p} \frac{dp}{dx}$
- Average value of  $2.1 \cdot 10^3 \text{ s}^{-1}$  within the metastable region
- Pressure and temperature return to saturated conditions once that the Wilson line is reached



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# DESIGNED NOZZLE: CFD RESULTS



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# CONCLUSIONS AND FUTURE WORK

- » The sCO<sub>2</sub> experimental test loop, which will allow the study of relevant phenomena taking place in the non-ideal gas region, is presented. The loop is under commissioning.
- » The results from the real-gas CFD simulation of the contraction zone indicate that no flow separation occurs, and a two-dimensional flow is provided to the supersonic test section.
- » The presented condensation model is validated and applied to the designed nozzle. The model assume a linear relation between the compressibility factor and pressure around the saturation pressure.
- » The effects of the low surface tension on condensation can be further studied and new condensation models can be developed considering the gas as non-ideal, i.e. compressibility factor lower than 1.

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# DESIGNED NOZZLE: CFD RESULTS

